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Thermodynamic modelling of alkali-activated slag cements

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Keywords

Thermodynamic modelling; alkali-activated slag cement; C-A-S-H; phase diagram; layered double
hydroxide; zeolite

Abstract

This paper presents a thermodynamic modelling analysis of alkali-activated slag-based cements,
which are high performance and potentially low-CO₂ binders relative to Portland cement. The

thermodynamic database used here contains a calcium (alkali) aluminosilicate hydrate ideal solid solution model (CNASH_{ss}), alkali carbonate and zeolite phases, and an ideal solid solution model for a hydrotalcite-like Mg-Al layered double hydroxide phase. Simulated phase diagrams for NaOH- and Na₂SiO₃-activated slag-based cements demonstrate the high stability of zeolites and other solid phases in these materials. Thermodynamic modelling provides a good description of the chemical compositions and types of phases formed in Na₂SiO₃-activated slag cements over the most relevant bulk chemical composition range for these cements, and the simulated volumetric properties of the cement paste are consistent with previously measured and estimated values. Experimentally determined and simulated solid phase assemblages for Na₂CO₃-activated slag cements were also found to be in good agreement. These results can be used to design the chemistry of alkali-activated slag-based cements, to further promote the uptake of this technology and valorisation of metallurgical slags.

1. Introduction

Development of high performance and low CO₂ cement-based materials is needed to reduce the CO₂ footprint of the construction industry. Alkali-activated cements are formed through the reaction of a soluble alkali source (the ‘activator’), water and aluminosilicate precursors, which are often sourced as industrial by-products (Provis, 2014). Blast furnace slag is one such material, and forms an important component of many modern cements, including use as the main raw material in production of alkali-activated slag (AAS) cements (Provis and Bernal, 2014). The reactive component of blast furnace slag is a calcium-magnesium aluminosilicate glass that dissolves under the high pH conditions provided by the activator to form a hydrated phase assemblage that consolidates into a hardened binder. AAS-based cements are attractive solutions for waste valorisation and utilisation of industrial by-products, e.g. in immobilisation matrices for radioactive wastes (Bai et al., 2011), and can provide substantial CO₂ savings relative to Portland cement (PC)-based materials (McLellan et al., 2011).

Understanding the durability of alkali-activated cements is a key scientific challenge facing their commercial uptake and utilisation (van Deventer et al., 2012). Durability is intimately linked to the chemistry and microstructure of these cements, and thus depends on physicochemical factors including chemical shrinkage and the solid phase assemblage formed.

The main component of hardened AAS-based materials is a calcium (alkali) aluminosilicate hydrate (C-(N-)A-S-H) gel¹ that is poorer in Ca (molar Ca/Si ratio ≈ 1 (Shi et al., 2006)) and richer in Al (molar Al/Si ratio > 0.1 (Le Saoût et al., 2011; Myers et al., 2013; Richardson et al., 1994)) than the calcium (alumino)silicate hydrate (C-(A-)S-H) gel formed in hydrated PC (Taylor et al., 2010). The solid phase assemblage in AAS cements contains phases other than C-(N-)A-S-H gel, typically including Mg-Al layered double hydroxide (LDH) phases (Richardson et al., 1994; Wang and Scrivener, 1995) and aluminoferrite-mono (AFm) type phases including strätlingite (C₂ASH₈) (Ben Haha et al., 2012; Richardson et al., 1994; Wang and Scrivener, 1995), and calcium monocarboaluminate hydrate (C₄A \bar{c} H₁₁) in Na₂CO₃ (N \bar{c})-activated slag (N \bar{c} -AS) cement (Shi et al., 2006). Katoite (C₃AH₆) (Bonk et al., 2003), zeolites including gismondine and heulandite (Bernal et al., 2015; Bernal et al., 2011), and the third aluminate hydrate (TAH) (Myers et al., 2015a), which is described as a poorly ordered Al(OH)₃ phase (Taylor et al., 2010), may additionally form in AAS cements. Recently, evidence for the formation of alkali aluminosilicate (hydrate) (N-A-S(-H)) gels in AAS cement has been presented (Myers et al., 2015a; Myers et al., 2013); this phase is considered to be similar to the ‘geopolymer’ gels formed through alkali-activation of low-Ca raw materials (Provis et al., 2005).

Thermodynamic modelling can be used to predict the chemistry of hydrated/alkali-activated cements, assuming equilibrium between the solid reaction products and pore solution (Atkins et al., 1992; Lothenbach, 2010; Savage et al., 2011), which is critically important in understanding their long-term behaviour, e.g. in radioactive waste disposal applications (Glasser and Atkins, 1994). This approach

¹ The various alkalis that may be incorporated into C-(N-)A-S-H gel are all represented by Na here because the alkali source in an alkali-activated cement is typically Na-based. Cement chemistry notation is used throughout the text: C = CaO; S = SiO₂; A = Al₂O₃; N = Na₂O; H = H₂O; M = MgO; \bar{c} = CO₂; and \bar{s} = SO₃.

has been applied to AAS cements in the past (Lothenbach and Gruskovnjak, 2007), however the calcium silicate hydrate (C-S-H) thermodynamic model (Kulik and Kersten, 2001) used in that study does not explicitly define the uptake of Al and Na which is needed to fully describe C-(N-)A-S-H gel. Chemically complete definitions of Al chemistry in the thermodynamic models used to simulate the phases formed in AAS-based cements are important in enabling accurate prediction of the chemistry of these cements. The inclusion of alkalis as a key component in thermodynamic models for C-(N-)A-S-H gel is also important to enable correct description of the solubility relationships of this phase under the high pH conditions (>12) and alkali concentrations (tens to hundreds of mmol/L) relevant to the majority of cementitious materials (Myers et al., 2014).

The CNASH_{ss} thermodynamic model used in the current paper was recently developed (Myers et al., 2014) to formally account for Na and tetrahedral Al incorporated in Ca/Si < 1.3 C-(N-)A-S-H gel. Here, this thermodynamic model is used to simulate the chemistry of AAS cements activated by aqueous solutions of NaOH ((NH)_{0.5}), Na₂SiO₃ (NS), Na₂Si₂O₅ (NS₂) and N_C. This thermodynamic model can describe a large set of solubility data for the CaO-(Na₂O,Al₂O₃)-SiO₂-H₂O and AAS cement systems, and closely matches the published chemical compositions of calcium aluminosilicate hydrate (C-A-S-H) gel, and the volumetric properties of C-(N-)A-S-H gel measured in a sodium silicate-activated slag cement (Myers et al., 2014). The CNASH_{ss} thermodynamic model is assessed here in terms of the prediction of solid phase assemblages and the Al content of C-(N-)A-S-H gel over the bulk slag chemical composition range which is most relevant to AAS cement-based materials. These simulations are performed using the Gibbs energy minimisation software GEM-Selektor v.3 (<http://gems.web.psi.ch/>) (Kulik et al., 2013; Wagner et al., 2012) and an expanded thermodynamic database for cements, based on the CEMDATA07 database (Babushkin et al., 1985; Hummel et al., 2002; Lothenbach et al., 2008; Lothenbach and Winnefeld, 2006; Matschei et al., 2007; Möschner et al., 2008; Möschner et al., 2009; Schmidt et al., 2008; Thoenen and Kulik, 2003) with the addition of an updated definition of Mg-Al LDH intercalated with OH⁻ (MA-OH-LDH), and including some zeolites and alkali carbonates. The results are discussed in terms of implications for the design of high performance AAS-based cements.

2. Methods

2.1 Thermodynamic model for C-(N-)A-S-H gel

The CNASH_{ss} thermodynamic model (Myers et al., 2014) is formulated as an ideal solid solution with mixing on six of eight sublattice sites to give three C-S-H gel end-members, one calcium (alkali) silicate hydrate (C-(N-)S-H) gel end-member, two C-A-S-H gel end-members and two C-(N-)A-S-H gel end-members (Table 1). End-member chemical compositions are defined in this model by extension of the ‘Substituted General Model’ (Richardson and Groves, 1993) for consistency with tobermorite-like nanostructures containing no ‘interstratified Ca(OH)₂’ (Richardson, 2004), which limits the applicability of the CNASH_{ss} thermodynamic model to Ca/Si ratios <1.3 in the C-(N-)A-S-H gel. Pentahedral Al (Al[5]) and octahedral Al (Al[6]) are not explicitly considered in the end-member structures described by CNASH_{ss}.

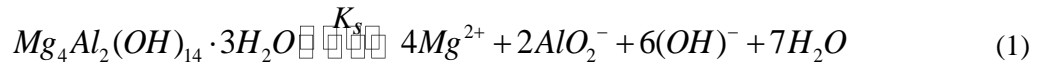
C-(N-)A-S-H gel is formally described in terms of non-cross-linked chain structures in the CNASH_{ss} thermodynamic model, but without precluding representation of cross-linked tobermorite-like chain structures, because these structural types cannot be differentiated by bulk chemical composition alone. Thermodynamic calculations using the CNASH_{ss} thermodynamic model are therefore also consistent with cross-linked C-(N-)A-S-H gel structural models such as those described by the ‘Cross-linked Substituted Tobermorite Model’ (CSTM) (Myers et al., 2013). Full details of the development and implementation of the CNASH_{ss} thermodynamic model are given in (Myers et al., 2014).

2.2 Thermodynamic model for MA-OH-LDH

Thermodynamic data for MA-OH-LDH were reformulated into an ideal solid solution thermodynamic model (MA-OH-LDH_{ss}) containing three end-members with Mg/Al ratios of 2, 3 and 4 (Table 1) to

match the known chemical composition range of this solid solution ($\text{Mg}_{(1-x)}\text{Al}_x(\text{OH})_{(2+x)} \cdot m\text{H}_2\text{O}$, $0.2 \leq x \leq 0.33$ (Richardson, 2013)).

Recalculation of recently published solubility data for $\text{Mg}/\text{Al} = 2$ MA-OH-LDH (M_4AH_{10}) (Gao and Li, 2012) and existing solubility data for this phase (Bennett et al., 1992) was performed in GEM-Selektor v.3 (<http://gems.web.psi.ch/>) (Kulik et al., 2013; Wagner et al., 2012) using the dissolution reaction eq.(1):



where K_s is the solubility product. Solubility data for this phase were also calculated using the additivity method (Anderson and Crerar, 1993) with brucite ($\text{Mg}(\text{OH})_2$ (s)), magnesite (MgCO_3 (s)) (Table 1), and hydrotalcite ($\text{Mg}_{0.74}\text{Al}_{0.26}(\text{OH})_2(\text{CO}_3)_{0.13} \cdot 0.39\text{H}_2\text{O}$ (s)) (Allada et al., 2005) constituents.

The recalculation results indicate that the solubility product used previously by Lothenbach and Winnefeld (2006) to describe this phase ($\log_{10}(K_s) = -56.02$ at 25°C and 1 bar), taken from the low solubility data reported by Bennett et al. (1992), is not consistent with the solubility data reported by Gao and Li (Gao and Li, 2012) (Figure 1). Here, a solubility product of $\log_{10}(K_s) = -49.70$ at 25°C and 1 bar is selected for improved consistency with the solubility data reported by Gao and Li (Gao and Li, 2012). The standard heat capacity and entropy of this phase are adapted from the thermodynamic data reported by Allada et al. (Allada et al., 2005) for $\text{Mg}_{0.74}\text{Al}_{0.26}(\text{OH})_2(\text{CO}_3)_{0.13} \cdot 0.39\text{H}_2\text{O}$ using the additivity method with $\text{Mg}(\text{OH})_2$ (s) and MgCO_3 (s) constituents, i.e. the standard heat capacity for M_4AH_{10} is calculated via eq.(2):

$$Cp^\circ_{\text{M}_4\text{AH}_{10}} = 2 \left(\frac{1}{0.26} Cp^\circ_{\text{Mg}_{0.74}\text{Al}_{0.26}(\text{OH})_2(\text{CO}_3)_{0.13} \cdot 0.39\text{H}_2\text{O}} - 0.5 Cp^\circ_{\text{MgCO}_3} - 0.346 Cp^\circ_{\text{Mg}(\text{OH})_2} \right) \quad (2)$$

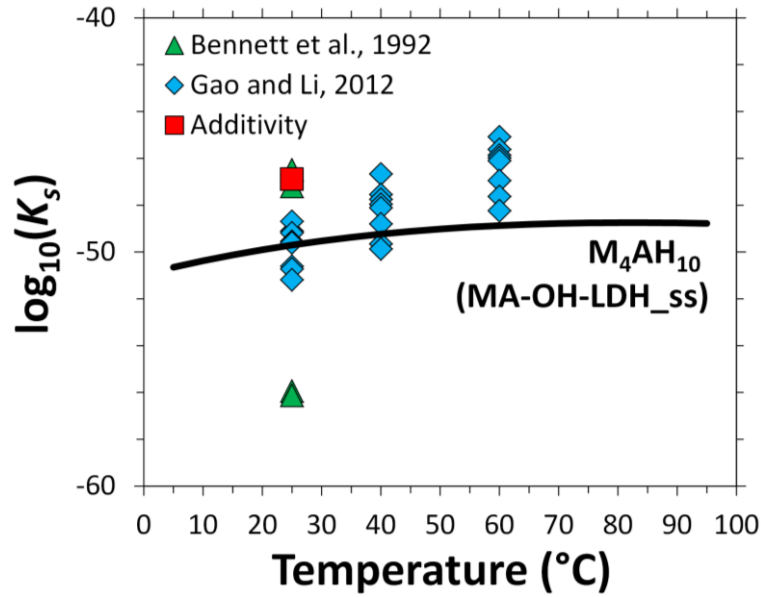


Figure 1. Comparison between the recalculated solubility data (Bennett et al., 1992; Gao and Li, 2012), results using the additivity method, and calculated solubility of the M_4AH_{10} end-member of the MA-OH-LDH_{ss} thermodynamic model used in this work (thick black line) ($P = 1$ bar). The green triangles at $\log_{10}(K_s) = -56.02$ (25°C and 1 bar), represents the solubility product used previously to describe this phase in the cement chemistry literature.

Standard entropies and heat capacities for $Mg/Al = 3$ MA-OH-LDH (M_6AH_{12}) and $Mg/Al = 4$ MA-OH-LDH (M_8AH_{14}) were determined in the same manner (using solid constituents and a reaction analogous to eq.(2)), using the thermodynamic data reported by Allada et al. (Allada et al., 2005). A difference of $-22.32 \log_{10}$ units was specified between the solubility products of M_4AH_{10} ($\log_{10}(K_s) = -49.70$) and M_6AH_{12} ($\log_{10}(K_s) = -72.02$), and between those of M_6AH_{12} and M_8AH_{14} ($\log_{10}(K_s) = -94.34$) at 25°C and 1 bar, which is the difference between the solubility products of these phases when determined using the additivity method described here. A similar difference is found between reported thermodynamic data for MA- ζ -LDH ($Mg_4Al_2(OH)_{12}(CO_3) \cdot 4H_2O$, $\log_{10}(K_s) = -44.19$ (Rozov et al., 2011) and $Mg_6Al_2(OH)_{16}(CO_3) \cdot 5H_2O$, $\log_{10}(K_s) = -66.58$ (Rozov, 2010)), which suggests that the additivity approach is appropriate for these structurally-similar Mg-Al LDH phases. The three MA-OH-LDH phases M_4AH_{10} , M_6AH_{12} and M_8AH_{14} were specified as end-members of the ideal solid solution 'MA-OH-LDH_{ss}'. This is justified because it has been shown that the assumption of mechanical (ideal) mixing is appropriate for modelling the total solubility of the structurally-similar hydrotalcite-pyroaurite solid solution series (Rozov et al., 2011). This MA-OH-LDH solid solution model is used in the thermodynamic modelling performed in this work.

179

180 **2.3 Occurrence of Mg, Fe and S-bearing phases**

181 Thermodynamic modelling of AAS cements requires consideration of additional constituent elements
182 outside the CaO-Na₂O-Al₂O₃-SiO₂-H₂O system, most notably Mg, Fe and S, as well as carbonates.
183 While the precipitation of Mg in AAS cement is generally well explained by its incorporation into
184 Mg-Al LDH phases (Ben Haha et al., 2011b; Richardson et al., 1994; Wang and Scrivener, 1995),
185 there is less consensus regarding the precipitation of Fe and S. Fe was excluded from this work,
186 consistent with the passivated state of this element in GBFS (Bernal et al., 2014a), and S released by
187 the slag was represented as S²⁻ with its oxidation limited by using a simulated N_{2(g)} atmosphere in the
188 thermodynamic modelling calculations.

189

190 **2.4 Other solid phases**

191 Thermodynamic data for cement-related solid phases other than C-(N-)A-S-H gel and MA-OH-LDH
192 were taken from the PSI/Nagra 12/07 thermodynamic database (Thoenen et al., 2013) and the
193 CEMDATA07 thermodynamic database, which was updated to include recently published data for
194 Al(OH)₃ and hydrogarnet phases (Dilnesa et al., 2014; Lothenbach et al., 2012) (Table 1).

195

196

Table 1. Thermodynamic properties of solid phases at 298.15 K and 1 bar.

| Phases ^a | V^\bullet (cm ³ mol ⁻¹) | ΔH_f^\bullet (kJ mol ⁻¹) | ΔG_f^\bullet (kJ mol ⁻¹) | S^\bullet (J mol ⁻¹ K ⁻¹) | C_p^\bullet (J mol ⁻¹ K ⁻¹) | Reference |
|--|--|--|--|--|--|--|
| $\frac{1}{2}\text{AH}_3$ (microcrystalline) | 32.0 | -1265 | -1148 | 140 | 93.1 | (Lothenbach et al., 2012) |
| Portlandite, CH | 33.1 | -985 | -897 | 83.4 | 87.5 | (Robie and Hemingway, 1995) |
| SiO ₂ (amorphous) | 29.0 | -903 | -849 | 41.3 | 44.5 | (Helgeson et al., 1978; Kulik and Kersten, 2001) |
| C ₂ AH ₈ | 90.1 | -5278 | -4696 | 450 | 521 | (Lothenbach et al., 2012) |
| Katoite, (C ₃ AH ₆) | 150 | -5537 | -5008 | 422 | 446 | (Lothenbach et al., 2012) |
| C ₄ AH ₁₉ | 382 | -1002 | -8750 | 1120 | 1382 | (Lothenbach et al., 2012) |
| CAH ₁₀ | 194 | -5288 | -4623 | 610 | 668 | (Lothenbach et al., 2012) |
| Strätlingite, C ₂ ASH ₈ | 216 | -6360 | -5705 | 546 | 603 | (Matschei et al., 2007) |
| Calcium monocarboaluminate hydrate, C ₄ A _{0.5} H ₁₁ | 262 | -8250 | -7337 | 657 | 881 | (Matschei et al., 2007) |
| Calcium hemicarboaluminate hydrate, C ₄ A _{0.5} H ₁₂ | 285 | -8270 | -7336 | 713 | 906 | (Matschei et al., 2007) |
| Calcium tricarboaluminate hydrate, C ₆ A _{0.5} H ₃₂ | 650 | -16792 | -14566 | 1858 | 2121 | (Matschei et al., 2007) |
| Ettringite, C ₆ A ₃ H ₃₂ | 707 | -17535 | -15206 | 1900 | 2174 | (Lothenbach et al., 2008) |
| Gypsum, C ₂ H ₂ | 74.7 | -2023 | -1798 | 194 | 186 | (Hummel et al., 2002; Thoenen et al., 2013) |
| Anhydrite, C ₂ | 45.9 | -1435 | -1322 | 107 | 99.6 | (Hummel et al., 2002; Thoenen et al., 2013) |
| Lime, C | 16.8 | -635 | -604 | 39.7 | 42.8 | (Helgeson et al., 1978) |
| Brucite, MH | 24.6 | -923 | -832 | 63.1 | 77.3 | (Helgeson et al., 1978; Hummel et al., 2002; Thoenen et al., 2013) |
| MA-c-LDH, M ₄ A _{0.5} H ₉ | 220 | -7374 | -6580 | 551 | 647 | (Lothenbach et al., 2008) |
| C-(N-)A-S-H gel ideal solid solution end-members, 'CNASH_ss' (Myers et al., 2014) | | | | | | |
| 5CA, C _{1.25} A _{0.125} S ₁ H _{1.625} | 57.3 | -2491 | -2293 | 163 | 177 | (Myers et al., 2014) |
| INFCA, C ₁ A _{0.15625} S _{1.1875} H _{1.65625} | 59.3 | -2551 | -2343 | 154 | 181 | (Myers et al., 2014) |
| 5CNA, C _{1.25} N _{0.25} A _{0.125} S ₁ H _{1.375} | 64.5 | -2569 | -2382 | 195 | 176 | (Myers et al., 2014) |
| INFCNA, C ₁ N _{0.34375} A _{0.15625} S _{1.1875} H _{1.3125} | 69.3 | -2667 | -2474 | 198 | 180 | (Myers et al., 2014) |
| INFCN, C ₁ N _{0.3125} S _{1.5} H _{1.1875} | 71.1 | -2642 | -2452 | 186 | 184 | (Myers et al., 2014) |
| T2C*, C _{1.5} S ₁ H _{2.5} ^b | 80.6 | -2721 | -2465 | 167 | 237 | (Myers et al., 2014) |
| T5C*, C _{1.25} S _{1.25} H _{2.5} ^b | 79.3 | -2780 | -2517 | 160 | 234 | (Myers et al., 2014) |

| | | | | | | |
|--|-------------------|--------|-------|------|----------------|--|
| TobH*, C ₁ S _{1.5} H _{2.5} ^b | 85.0 | -2831 | -2560 | 153 | 231 | 2014) (Myers et al., 2014) |
| Calcium monosulfoaluminate-hydroxoaluminate hydrate non-ideal solid solution (Matschei et al., 2007) | | | | | | |
| Calcium monosulfoaluminate hydrate, C ₄ A ₅ H ₁₂ | 309 | -8750 | -7779 | 821 | 942 | (Matschei et al., 2007) |
| C ₄ AH ₁₃ | 274 | -8300 | -7324 | 700 | 930 | (Lothenbach et al., 2012) |
| MA-OH-LDH ideal solid solution end-members, 'MA-OH-LDH_ss' | | | | | | |
| M ₄ AH ₁₀ | 219 | -7160 | -6358 | 549 | 648 | (Allada et al., 2005; Richardson, 2013) |
| M ₆ AH ₁₂ | 305 | -9007 | -8023 | 675 | 803 | This study ^c |
| M ₈ AH ₁₄ | 392 | -10853 | -9687 | 801 | 958 | This study ^c |
| Carbonates | | | | | | |
| Aragonite, C _c | 34.2 | -1207 | -1128 | 90.2 | 81.3 | (Hummel et al., 2002; Thoenen et al., 2013) |
| Calcite, C _c | 36.9 | -1207 | -1129 | 92.7 | 81.9 | (Hummel et al., 2002; Thoenen et al., 2013) |
| Dolomite (disordered), CM _c C ₂ | 64.4 | -2317 | -2157 | 167 | 158 | (Hummel et al., 2002; Thoenen et al., 2013) |
| Natron, N _c H ₁₀ | 197 | -4079 | -3428 | 563 | 550 | (Königsberger et al., 1999; Taga, 1969) |
| Gaylussite, NC _c C ₂ H ₅ | 149 | -3834 | -3372 | 387 | - ^d | (Dickens and Brown, 1969; Königsberger et al., 1999) |
| Pirssonite, NC _c C ₂ H ₂ | 104 | -2956 | -2658 | 239 | 329 | (Dickens and Brown, 1969; Königsberger et al., 1999) |
| Magnesite, M _c | 28.0 | -1113 | -1029 | 65.7 | 75.8 | (Hummel et al., 2002; Thoenen et al., 2013) |
| Huntite, CM ₃ C ₄ | 123 | -4533 | -4206 | 300 | 310 | (Graf and Bradley, 1962; Hemingway and Robie, 1972; Königsberger et al., 1999) |
| Artinite, M ₂ C ₄ H ₄ | 96.2 | -2921 | -2568 | 233 | 248 | (de Wolff, 1952; Hemingway and Robie, 1972; Königsberger et al., 1999) |
| Lansfordite, M _c H ₅ | 103 | -2574 | -2198 | 250 | 386 | (Hill et al., 1982; Königsberger et al., 1999) |
| Zeolites | | | | | | |
| Na-analcime, [Na _{0.32}].[Al _{0.32} Si _{0.68} O ₂].0.333H ₂ O | 32.5 ^c | -1099 | -1026 | 75.6 | 70.5 | (Johnson et al., 1982) |

| | | | | | | |
|---|-------------------|-------|-------|-------------------|-------------------|-------------------------|
| Natrolite, $[\text{Na}_{0.4}][\text{Al}_{0.4}\text{Si}_{0.6}\text{O}_2].0.4\text{H}_2\text{O}$ | 33.8 ^c | -1144 | -1063 | 71.9 | 60.4 | (Johnson et al., 1983) |
| Ca-heulandite, $[\text{Ca}_{0.111}][\text{Al}_{0.222}\text{Si}_{0.778}\text{O}_2].0.667\text{H}_2\text{O}$ | 35.2 ^e | -1179 | -1090 | 87.1 | 82.9 | (Kiseleva et al., 2001) |
| (Ca,Na)-heulandite, $[\text{Ca}_{0.111}\text{Na}_{0.028}][\text{Al}_{0.25}\text{Si}_{0.75}\text{O}_2].0.667\text{H}_2\text{O}$ | 35.2 ^e | -1185 | -1094 | 84.0 | 82.9 | (Kiseleva et al., 2001) |
| Basic sodalite, $[\text{Na}_{0.65}(\text{OH})_{0.15}][\text{Al}_{0.5}\text{Si}_{0.5}\text{O}_2].0.27\text{H}_2\text{O}$ | 35.0 ^e | -1190 | -1106 | 67.8 ^f | 66.7 ^f | (Moloy et al., 2006) |

^a Cement chemistry notation is used: C = CaO; S = SiO₂; A = Al₂O₃; H = H₂O; N = Na₂O; M = MgO; $\underline{\text{c}}$ = CO₂; $\underline{\text{s}}$ = SO₃.

^b The asterisks for the T2C*, T5C* and TobH* end-members indicate that these components have slightly modified thermodynamic properties but the same chemical composition relative to the T2C, T5C and TobH end-members of the downscaled CSH3T thermodynamic model (Kulik, 2011).

^c Thermodynamic properties based on the thermochemical data in (Allada et al., 2005) and solubility data in (Bennett et al., 1992; Gao and Li, 2012), section 2.2, with molar volumes calculated from (Richardson, 2013).

^d Not available

^e Molar volumes calculated from framework densities, lattice types and lattice cell parameters for each zeolite framework type (Baerlocher et al., 2007).

^f Standard entropy and heat capacity estimated using the additivity method (Anderson and Crerar, 1993) based on H₂O_(l) (Table 2), gibbsite (Helgeson et al., 1978; Hummel et al., 2002), NaOH_(s) (Robie and Hemingway, 1995) and amorphous SiO₂ (Table 1).

Thermodynamic data for some zeolites and alkali carbonate minerals were used to provide a preliminary assessment of the stability of these phases in AAS cements (Table 1) and should be treated as provisional only, because the thermodynamic data were not recompiled for full internal consistency with the Nagra-PSI and CEMDATA07 thermodynamic databases. Reliable thermodynamic data for other Na-carbonates which can form in AAS cements (i.e. natrite, thermonatrite, nahcolite and trona) were not available (Königsberger et al., 1999; Monnin and Schott, 1984), and so were not included in the simulations.

The formation of siliceous hydrogarnet was suppressed in the simulations because this phase does not tend to form at ambient temperature and pressure, possibly for kinetic reasons (Lothenbach et al., 2008). No additional restrictions related to the formation of any other solid phases shown in Table 1 were specified.

2.5 Approach

Thermodynamic modelling was performed using the Gibbs energy minimisation software GEM-Selektor v.3 (<http://gems.web.psi.ch/>) (Kulik et al., 2013; Wagner et al., 2012), with thermodynamic data for the solid phases shown in Table 1 and thermodynamic data for aqueous species/complexes and gases shown in Tables 2 and 3, respectively. The Truesdell-Jones form of the extended Debye-Hückel equation (eq.(3)) (Helgeson et al., 1981) and the ideal gas equation of state were used for the aqueous and gaseous phase models, respectively, with the average ion size (\bar{a} , Å) and the parameter for common short-range interactions of charged species (b_γ , kg mol⁻¹) specified to represent NaOH-dominated solutions (3.31 Å and 0.098 kg mol⁻¹, respectively (Helgeson et al., 1981)).

$$\log_{10} \gamma_j = \frac{-A_\gamma z_j^2 \sqrt{I}}{1 + \bar{a} B_\gamma \sqrt{I}} + b_\gamma I + \log_{10} \frac{x_{jw}}{X_w} \quad (3)$$

The parameters γ_j and z_j in eq.(3) are the activity coefficient and charge of the j^{th} aqueous species, respectively, A_γ (kg^{0.5} mol^{-0.5}) and B_γ (kg^{0.5} mol^{-0.5} cm⁻¹) are T,P-dependent electrostatic parameters, I is the ionic strength of the aqueous electrolyte phase (mol kg⁻¹), x_{jw} (mol) is the molar quantity of water and X_w (mol) is the total molar amount of the aqueous phase. The activity of water is calculated from the osmotic coefficient (Helgeson et al., 1981) and unity activity coefficients for neutral dissolved species are used.

Table 2. Thermodynamic properties of the aqueous species used in the thermodynamic modelling simulations.

| Species/complex ^a | V^\bullet (cm ³ mol ⁻¹) | ΔH_f^\bullet (kJ mol ⁻¹) | ΔG_f^\bullet (kJ mol ⁻¹) | S^\bullet (J mol ⁻¹ K ⁻¹) | C_p^\bullet (J mol ⁻¹ K ⁻¹) | Reference |
|---|--|--|--|--|--|----------------------|
| Al ³⁺ | -45.2 | -530.6 | -483.7 | -325.1 | -128.7 | (Shock et al., 1997) |
| AlO ⁺ (+ H ₂ O = Al(OH) ₂ ⁺) | 0.3 | -713.6 | -660.4 | -113 | -125.1 | (Shock et al., 1997) |
| AlO ₂ ⁻ (+ 2H ₂ O = Al(OH) ₄ ⁻) | 9.5 | -925.6 | -827.5 | -30.2 | -49 | (Shock et al., 1997) |
| AlOOH ^o (+ 2H ₂ O = Al(OH) ₃ ^o) | 13 | -947.1 | -864.3 | 20.9 | -209.2 | (Shock et al., 1997) |
| AlOH ²⁺ | -2.7 | -767.3 | -692.6 | -184.9 | 56 | (Shock et al., 1997) |

| | | | | | | |
|--|-------|--------|--------|--------|--------|---|
| $\text{AlHSiO}_3^{2+} (+ \text{H}_2\text{O} = \text{AlSiO}(\text{OH})_3^{2+})$ | -40.7 | -1718 | -1541 | -304.2 | -215.9 | 1997) (Matschei et al., 2007) |
| $\text{AlSiO}_4^- (+ 3\text{H}_2\text{O} = \text{AlSiO}(\text{OH})_6^-)$ | 25.5 | -1834 | -1681 | 11.1 | -4.6 | (Matschei et al., 2007) |
| AlSO_4^+ | -6.0 | -1423 | -1250 | -172.4 | -204.0 | (Matschei et al., 2007) |
| $\text{Al}(\text{SO}_4)_2^-$ | 31.1 | -2338 | -2006 | -135.5 | -268.4 | (Matschei et al., 2007) |
| Ca^{2+} | -18.4 | -543.1 | -552.8 | -56.5 | -30.9 | (Shock et al., 1997) |
| CaOH^+ | 5.8 | -751.6 | -717 | 28 | 6 | (Shock et al., 1997) |
| $\text{CaHSiO}_3^+ (+ \text{H}_2\text{O} = \text{CaSiO}(\text{OH})_3^+)$ | -6.7 | -1687 | -1574 | -8.3 | 137.8 | (Sverjensky et al., 1997) |
| $\text{CaSiO}_3^0 (+ \text{H}_2\text{O} = \text{CaSiO}_2(\text{OH})_2^0)$ | 15.7 | -1668 | -1518 | -136.7 | 88.9 | (Matschei et al., 2007) |
| CaSO_4^0 | 4.7 | -1448 | -1310 | 20.9 | -104.6 | (Sverjensky et al., 1997) |
| CaCO_3^0 | -1.6 | -1202 | -1099 | 10.5 | -123.9 | (Sverjensky et al., 1997) |
| CaHCO_3^+ | 13.3 | -1232 | -1146 | 66.9 | 233.7 | (Hummel et al., 2002; Thoenen et al., 2013) |
| K^+ | 9.0 | -252.1 | -282.5 | 101 | 8.4 | (Shock et al., 1997) |
| KOH^0 | 15 | -474.1 | -437.1 | 108.4 | -85 | (Shock et al., 1997) |
| KSO_4^- | 27.5 | -1159 | -1032 | 146.4 | -45.1 | (Sverjensky et al., 1997) |
| Na^+ | -1.2 | -240.3 | -261.9 | 58.4 | 38.1 | (Shock et al., 1997) |
| NaOH^0 | 3.5 | -470.1 | -418.1 | 44.8 | -13.4 | (Shock et al., 1997) |
| NaSO_4^- | 18.6 | -1147 | -1010 | 101.8 | -30.1 | (Matschei et al., 2007) |
| NaCO_3^- | -0.4 | -938.6 | -797.1 | -44.3 | -51.3 | (Hummel et al., 2002; Thoenen et al., 2013) |
| NaHCO_3^0 | 32.3 | -929.5 | -847.4 | 154.7 | 200.3 | (Hummel et al., 2002; Thoenen et al., 2013) |
| $\text{HSiO}_3^- (+ \text{H}_2\text{O} = \text{SiO}(\text{OH})_3^-)$ | 4.5 | -1145 | -1014 | 20.9 | -87.2 | (Sverjensky et al., 1997) |
| $\text{SiO}_2^0 (+ 2\text{H}_2\text{O} = \text{Si}(\text{OH})_4^0)$ | 16.1 | -887.9 | -833.4 | 41.3 | 44.5 | (Kulik and Kersten, 2001; Shock et al., 1989) |
| $\text{SiO}_3^{2-} (+ \text{H}_2\text{O} = \text{SiO}_2(\text{OH})_2^{2-})$ | 34.1 | -1099 | -938.5 | -80.2 | 119.8 | (Matschei et al., 2007) |
| $\text{S}_2\text{O}_3^{2-}$ | 27.6 | -649.9 | -520.0 | 66.9 | -238.5 | (Shock et al., 1997) |
| HSO_3^- | 33.0 | -627.7 | -529.1 | 139.7 | -5.4 | (Shock et al., 1997) |
| SO_3^{2-} | -4.1 | -636.9 | -487.9 | -29.3 | -281.0 | (Shock et al., 1997) |

| | | | | | | |
|---|-------|---------|--------|--------|--------|---|
| | | | | | | 1997) |
| HSO_4^- | 34.8 | -889.2 | -755.8 | 125.5 | 22.7 | (Shock et al., 1997) |
| SO_4^{2-} | 12.9 | -909.7 | -744.5 | 18.8 | -266.1 | (Shock et al., 1997) |
| H_2S^0 | 35.0 | -39.0 | -27.9 | 125.5 | 179.2 | (Shock et al., 1997) |
| HS^- | 20.2 | -16.2 | 12.0 | 68.2 | -93.9 | (Shock et al., 1997) |
| S^{2-} | 20.2 | 92.2 | 120.4 | 68.2 | -93.9 | (Shock et al., 1997) |
| Mg^{2+} | -22.0 | -465.9 | -454.0 | -138.1 | -21.7 | (Shock et al., 1997) |
| MgOH^+ | 1.6 | -690.0 | -625.9 | -79.9 | 129.2 | (Shock et al., 1997) |
| $\text{MgHSiO}_3^+ (+ \text{H}_2\text{O} = \text{MgSiO}(\text{OH})_3^+)$ | -10.9 | -1614 | -1477 | -99.5 | 158.6 | (Shock et al., 1997) |
| MgSO_4^0 | 1.8 | -1369 | -1212 | -50.9 | -90.3 | (Hummel et al., 2002; Shock et al., 1997; Thoenen et al., 2013) |
| $\text{MgSiO}_3^0 (+ \text{H}_2\text{O} = \text{MgSiO}_2(\text{OH})_2^0)$ | 12.1 | -1597 | -1425 | -218.3 | 98.2 | (Hummel et al., 2002; Thoenen et al., 2013) |
| MgCO_3^0 | -16.7 | -1132 | -999.0 | -100.4 | -116.5 | (Hummel et al., 2002; Sverjensky et al., 1997; Thoenen et al., 2013) |
| MgHCO_3^+ | 9.3 | -1154.0 | -1047 | -12.6 | 254.4 | (Hummel et al., 2002; Thoenen et al., 2013) |
| CO_2^0 | 32.8 | -413.8 | -386.0 | 117.6 | 243.1 | (Hummel et al., 2002; Shock et al., 1989; Thoenen et al., 2013) |
| CO_3^{2-} | -6.1 | -675.3 | -528.0 | -50.0 | -289.3 | (Shock et al., 1997) |
| HCO_3^- | 24.2 | -690.0 | -586.9 | 98.5 | -34.8 | (Shock et al., 1997) |
| CH_4^0 | 37.4 | -87.8 | -34.4 | 87.8 | 277.3 | (Hummel et al., 2002; Shock and Helgeson, 1990; Thoenen et al., 2013) |
| OH^- | -4.7 | -230 | -157.3 | -10.7 | -136.3 | (Shock et al., 1997) |
| H^+ | 0 | 0 | 0 | 0 | 0 | (Shock et al., 1997) |
| H_2O^0 | 18.1 | -285.9 | -237.2 | 69.9 | 75.4 | (Johnson et al., 1992) |
| H_2^0 | 25.3 | -4.0 | 17.7 | 57.7 | 166.9 | (Hummel et al., |

2002; Shock et al., 1989; Thoenen et al., 2013) (Shock et al., 1989) (Shock et al., 1989)

| | | | | | |
|---------|------|-------|------|------|-------|
| N_2^o | 33.4 | -10.4 | 18.2 | 95.8 | 234.2 |
| O_2^o | 30.5 | -12.2 | 16.4 | 109 | 234.1 |

^a The hydration reactions shown in parentheses indicate hydrated species/complexes represented by the simulated aqueous species/complexes.

Table 3. Thermodynamic properties of the gases used in the thermodynamic modelling simulations.

| Gases | V^o (cm ³ mol ⁻¹) | ΔH_f^o (kJ mol ⁻¹) | ΔG_f^o (kJ mol ⁻¹) | S^o (J mol ⁻¹ K ⁻¹) | C_p^o (J mol ⁻¹ K ⁻¹) | Reference |
|------------------|--|--|--|--|--|-----------------------|
| N ₂ | 24790 | 0 | 0 | 191.6 | 29.1 | (Wagman et al., 1982) |
| O ₂ | 24790 | 0 | 0 | 205.1 | 29.3 | (Wagman et al., 1982) |
| H ₂ | 24790 | 0 | 0 | 130.7 | 28.8 | (Wagman et al., 1982) |
| CO ₂ | 24790 | -393.5 | -394.4 | 213.7 | 37.1 | (Wagman et al., 1982) |
| CH ₄ | 24790 | -74.8 | -50.7 | 186.2 | 35.7 | (Wagman et al., 1982) |
| H ₂ S | 24790 | -20.6 | -33.8 | 205.8 | 34.2 | (Wagman et al., 1982) |

Chemical equilibrium between the solid, aqueous and gaseous phases was assumed, and the simulated slag was specified to dissolve congruently at each particular bulk slag chemical composition. The assumption of congruent dissolution is valid for calcium aluminosilicate glasses of similar bulk chemical compositions to GBFS in highly under-saturated conditions at pH = 13 (Snellings, 2013). This condition is likely to be approximated in AAS cements when the solution pH is sufficiently high (Bernal et al., 2015), although it is clear that this assumption will need to be revisited in some systems, particularly for AAS cements cured for long times or synthesised with less basic activators such as Na₂CO₃ (Bernal et al., 2015).

Simulations of AAS cements were performed using 100 g slag, additions of H₂O, NaOH or Na₂O, SiO₂ and Na₂CO₃ to achieve fixed water to binder (w/b, where binder = slag + anhydrous activator

component) ratios of 0.4 and activator concentrations of 4 g Na₂O equivalent/100 g slag (the activators used are NaOH, Na₂SiO₃, Na₂Si₂O₅ and Na₂CO₃), a nitrogen atmosphere (10 mol N_{2(g)} per 100 g slag), and temperature/pressure conditions of 298.15 K and 1 bar. This simulation setup directly represents the AAS cements studied in (Bernal et al., 2015; Bernal et al., 2014b; Myers et al., 2015a; Myers et al., 2013), and is also similar to the AAS cement formulations reported in (Ben Haha et al., 2011b, 2012; Le Saoût et al., 2011) (which had ~3 mass% Na₂O equivalent and w/b = 0.4). With the exception of the phase diagram simulations (section 3.4), the simulated slag compositions are based on the GBFS composition shown in Table 4.

Table 4. Bulk chemical composition of the GBFS (from (Myers et al., 2015a)) used to specify the chemical compositions of the simulated slag in the thermodynamic modelling simulations.

| Component | Chemical composition (mass%) |
|--------------------------------|------------------------------|
| SiO ₂ | 33.8 |
| CaO | 42.6 |
| MgO | 5.3 |
| Al ₂ O ₃ | 13.7 |
| Na ₂ O | 0.1 |
| K ₂ O | 0.4 |
| SO ₃ ^a | 0.8 |
| Other | 1.5 |
| LOI ^b | 1.8 |
| Total | 100 |

^a S is represented in oxide form in standard XRF analysis, but S is treated as S²⁻ here (see section 2.2).

^b LOI is loss on ignition at 1000°C.

In section 3.1, the utility of the thermodynamic database (Tables 1-3) is assessed by using the slag composition given in Table 4 in terms of SiO₂, CaO, MgO, Al₂O₃, Na₂O, K₂O, and H₂S (corresponding to the “SO₃” content of the slag in Table 4) only, except for a variable oxide component (Al₂O₃, MgO or CaO), which was specified according to the simulation conducted. A simulated slag reaction extent of 60% was employed, which represents a typical degree of reaction quantified for GBFS in sodium silicate-activated slag cements (~48% at 180 days in (Ben Haha et al., 2011a), 54 ±3% at 100 days in (Le Saoût et al., 2011), 58-61% at 180 days in (Bernal et al., 2014b) and >70% after 1 month in (Myers et al., 2015a)). A density of 2.8 g/cm³ was selected for the unreacted slag component (Bernal et al., 2015).

Specific details pertaining to the descriptions of the slags simulated here, for each other aspect of the study, are shown near the beginning of each of sections 3.2-3.4.

3. Results and discussion

3.1 Utility of the CNASH_{ss} and MA-OH-LDH_{ss} thermodynamic models

Figure 2A shows that the calculated phase assemblage in NS-activated slag (NS-AS) cement changes as a function of Al₂O₃ content in the slag. The phase assemblage is dominated by C-(N-)A-S-H gel, in addition to MA-OH-LDH at all Al₂O₃ contents, and strätlingite, which also forms between 9 and 20 mass% Al₂O₃. Mg-Al LDH phases are commonly identified in sodium silicate-activated slag cements derived from slags with ≥ 5 mass% MgO (Bernal et al., 2014b), in good agreement with these results; LDH formation is reassessed in detail below. The simulated volume of the MA-OH-LDH phase does not change greatly here because its formation is limited by the amount of Mg supplied by the slag, which is constant at a fixed slag reaction extent. Small amounts of katoite are predicted for slags with 7-11 mass% Al₂O₃, which is relatively consistent with the observation of small amounts of this phase in sodium silicate-activated slag cements produced from slags with ~ 13 mass% Al₂O₃ (Bernal et al., 2014b; Schneider et al., 2001). Natrolite is predicted between 17 and 20 mass% slag Al₂O₃ content and very small quantities of brucite are predicted for slags with < 7 mass% Al₂O₃.

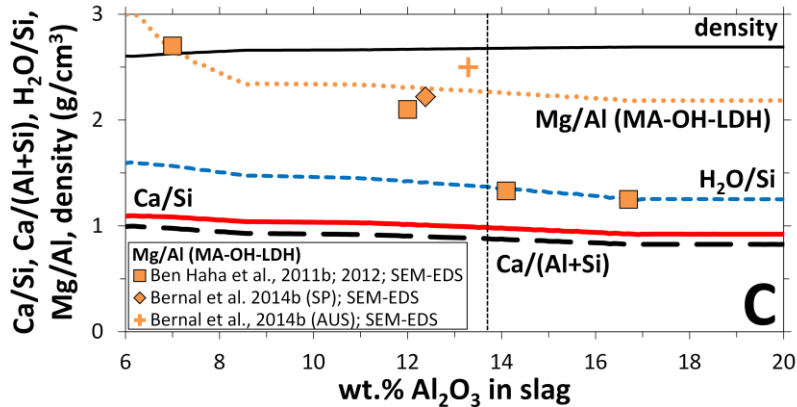
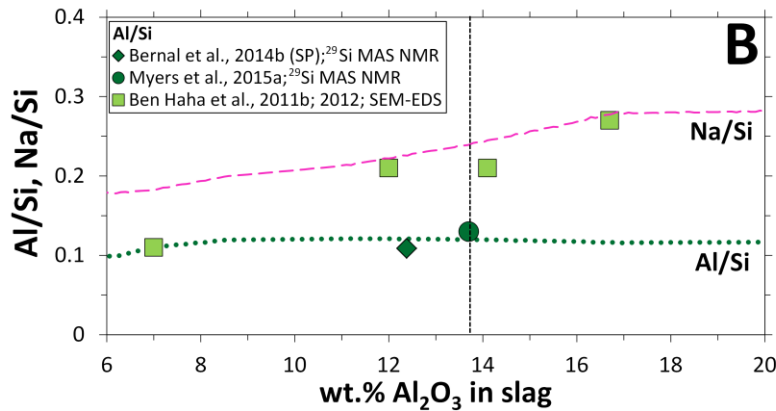
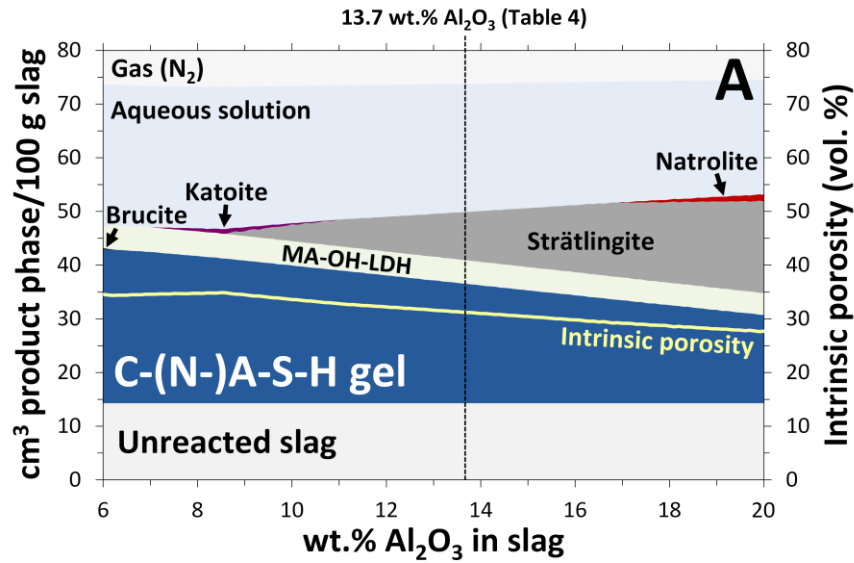


Figure 2. Simulated A) solid phase assemblages, B) Al/Si ratios in C-(N-)A-S-H gel, and C) Mg/Al ratios in MA-OH-LDH in NS-AS cements with bulk slag chemical compositions rescaled from Table 4 except for the Al_2O_3 content, which is varied here. Changes in B) Na/Si, C) $\text{H}_2\text{O}/\text{Si}$, Ca/Si and Ca/(Al+Si) ratios in C-(N-)A-S-H gel, and C) C-(N-)A-S-H gel density (g/cm^3) are shown for visual reference. The symbols in B) and C) are experimental results for sodium silicate-activated slag cements cured for 180 days and derived from slag precursors with similar MgO and equivalent or slightly lower CaO content ($5.2 < \text{mass\% MgO} < 7.7$, $35 < \text{mass\% CaO} \leq 42.6$) to the slag represented by Table 4.

The Mg/Al ratio of the simulated MA-OH-LDH phase is between 2 and 3 over the full range of simulated slag Al_2O_3 compositions (Figure 2C), in excellent agreement with experimentally determined Mg/Al ratios for this phase by scanning electron microscopy (SEM) with energy-dispersive X-ray spectroscopy (EDS) analysis in sodium silicate-activated slag cements for slags containing $7 \leq \text{mass\% Al}_2\text{O}_3 \leq 13.3$ (Ben Haha et al., 2012; Bernal et al., 2014b). However, the experimental SEM-EDS data suggest a systematic reduction in the Mg/Al ratio of this phase to below 2 as a function of increasing slag Al_2O_3 content (Ben Haha et al., 2012; Bernal et al., 2014b), that was not captured by the modelling performed here, as the MA-OH-LDH_{ss} thermodynamic model only describes solid solutions in the range $2 \leq \text{Mg/Al} \leq 4$. Regions with Mg/Al ratios < 2 identified in transmission electron microscopy (TEM)-EDS analysis of hydrated PC/GBFS cements (Taylor et al., 2010) are discussed in terms of intimate mixtures of Mg-Al LDH and $\text{Al}(\text{OH})_3$ -type phases because the chemical composition of Mg-Al LDH is theoretically limited to the range modelled here, $2 \leq \text{Mg/Al} \leq 4$ (Richardson, 2013). The experimental Mg/Al ratios < 2 shown in Figure 2C can thus be described similarly, which would explain the difference between the modelled and experimentally measured data. This analysis suggests a need for additional thermodynamic data describing Al-rich and Mg-poor solid phases that are not currently included in the thermodynamic database (e.g. TAH (Andersen et al., 2006)) rather than a deficiency in the MA-OH-LDH_{ss} thermodynamic model as such.

The amount of C-(N-)A-S-H gel formed in the simulated NS-AS cements decreases with increasing Al_2O_3 content of the slag (Figure 2A) at the expense of strätlingite precipitation. An Al/Si ratio ≈ 0.12 is calculated for C-(N-)A-S-H gel in NS-AS cements derived from slags with $>8 \text{ mass\% Al}_2\text{O}_3$ (Figure 2B), which corresponds closely to the Al/Si ratios determined for this phase by analysis of deconvoluted ^{29}Si magic angle spinning nuclear magnetic resonance (MAS NMR) spectra for these materials at 180 days of age (Bernal et al., 2014b; Myers et al., 2015a) using the CSTM (Myers et al., 2013). The CSTM is a structural model that represents C-(N-)A-S-H gel in terms of mixed cross-linked/non-cross-linked components that enables chemical compositions and structural parameters to be determined from deconvolution analysis of ^{29}Si MAS NMR spectra for materials containing this

phase. However, the experimental Al/Si ratios determined from ^{29}Si MAS NMR shown here exclude the potential uptake of Al[5] (Andersen et al., 2006) and Al[6] (Sun et al., 2006) in C-(N-)A-S-H gel, so are expected to be slightly lower than the ‘true’ Al/Si ratio in this phase. This discrepancy is discussed further in section 3.2. However, the much higher Al/Si ratios shown by the other SEM-EDS data, with $\text{Mg}/\text{Al} < 2$, could indicate mixtures of C-(N-)A-S-H gel with Mg-free and Al-containing phases in the interaction volumes analysed by SEM-EDS. This description is similar to the analysis above for Mg-Al LDH, so the thermodynamic modelling results are not necessarily inconsistent with these experimental SEM-EDS data.

The total binder volume (solid + aqueous phases) is calculated to be approximately constant over the full range of slag Al_2O_3 compositions studied (Figure 2A), suggesting that the bulk Al content of the slag in NS-AS cements should not greatly affect the chemical shrinkage properties of these materials. The results indicate a 20% change in intrinsic porosity (defined as the ratio of aqueous phase volume to total binder volume, where water chemically bound in, or adsorbed to, the solid phases described in Table 1 is considered to be a component of the solid) for slag compositions between ~8 and 20 mass% Al_2O_3 . This interpretation corresponds to the simulated C-(N-)A-S-H gel density of 2.5-2.7 g/cm³ and $\text{H}_2\text{O}/\text{Si}$ ratios between 1.3 and 1.7 (in agreement with C-(N-)A-S-H gel at $\text{RH} \approx 25\%$ (Muller et al., 2013)), as shown in Figure 2C. Therefore, this phase is conceptually equivalent to C-(N-)A-S-H gel with interlayer and some adsorbed water but no ‘gel’ or ‘free’ water (Jennings, 2008). However, the reduced intrinsic porosity found here at higher bulk slag Al_2O_3 content does not explain the weak dependency of sodium silicate-activated slag cement compressive strengths on bulk slag Al_2O_3 content (Ben Haha et al., 2012), because an increase in compressive strength would be expected at lower porosity. This discrepancy is attributed to the higher amount of strätlingite simulated here compared to the amount of this phase which is identified in AAS cements; this issue is revisited in section 3.2.

Simulations of NS-AS cements derived from slags with 0-18 mass% MgO (Figure 3) show little change in intrinsic porosity and total binder volume as a function of MgO content. This result differs

from previous thermodynamic modelling that showed a significant increase in total solid volume over this same MgO composition range (Ben Haha et al., 2011b). This difference is partly founded in the high amounts of strätlingite predicted, but also relates to the use of the CNASH_{ss} thermodynamic model here, rather than the less complex thermodynamic model used to describe C-(N-)A-S-H gel by Ben Haha et al. (2011b) (density $\approx 2.2\text{-}2.4\text{ g/cm}^3$ (Lothenbach et al., 2008)), as the current work formally defines the uptake of Al in C-(N-)A-S-H gel and much more closely describes the volumetric properties of this phase in sodium silicate-activated slag cement (density = $2.6\text{-}2.7\text{ g/cm}^3$ in Figure 3C, compared to $2.73 \pm 0.02\text{ g/cm}^3$ reported by Thomas et al. (2012)).

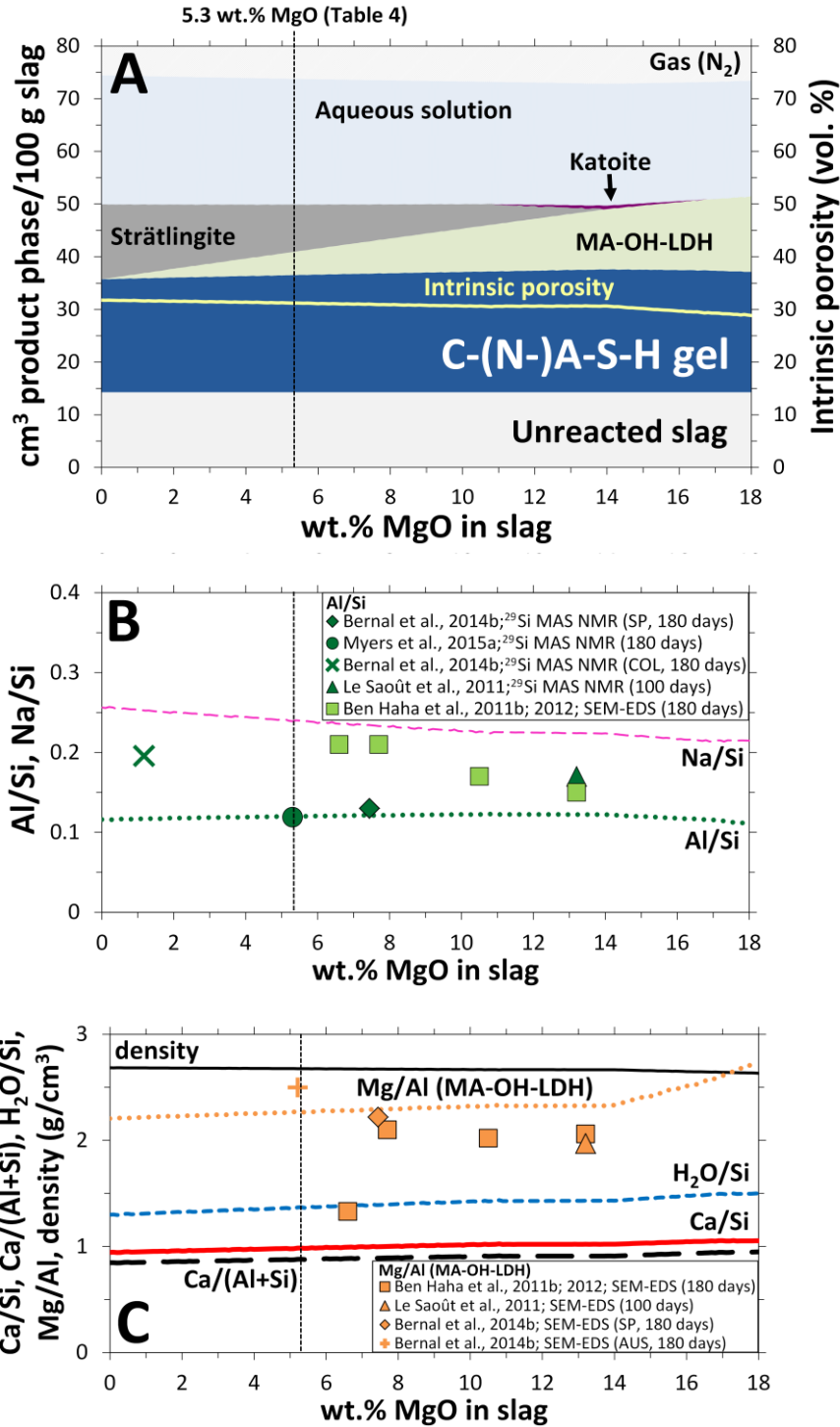


Figure 3. Simulated A) solid phase assemblages, B) Al/Si ratios in C-(N-)A-S-H gel, and C) Mg/Al ratios in MA-OH-LDH in NS-AS cements with bulk slag chemical compositions rescaled from Table 4 except for the Mg content, which is varied here. Changes in B) Na/Si, C) H₂O/Si, Ca/Si and Ca/(Al+Si) ratios in C-(N-)A-S-H gel, and C) C-(N-)A-S-H gel density (g/cm³) are shown for visual reference. The symbols in B) and C) represent experimentally measured data for sodium silicate-activated slag cements (curing times are indicated in parentheses) derived from slag precursors with similar Al₂O₃ and equivalent or slightly lower CaO content (11.3 < mass% Al₂O₃ < 14.1, 33.4 < mass% CaO ≤ 42.6) to the slag represented by Table 4.

The solid phase assemblage changes markedly as a function of the MgO content of the slag (Figure 3A), but little change in C-(N-)A-S-H gel volume is simulated between 0 and 18 mass% MgO. The only Mg-bearing solid phase predicted is MA-OH-LDH, the amount of which increases as a function of the slag MgO content. The simulated and experimentally measured Mg/Al ratios of this phase in sodium silicate-activated slag cements are consistent to ± 0.3 units (simulated Mg/Al ≈ 2.3 , Figure 3C) (Ben Haha et al., 2011b; Bernal et al., 2014b; Le Saoût et al., 2011), with the exception of the samples containing significant intermixing of additional products (with Mg/Al $\ll 2$). This result further supports the thermodynamic description of MA-OH-LDH used here. The only predicted minor phase is katoite at 11-17 mass% MgO. Brucite is not predicted here, in good agreement with its absence from experimentally observed solid phase assemblages in AAS cements (Ben Haha et al., 2011b; Myers et al., 2015a; Richardson et al., 1994; Schneider et al., 2001; Wang and Scrivener, 1995).

The Al/Si ratio of the simulated C-(N-)A-S-H gel (Al/Si ≈ 0.12) is similar to the experimentally determined Al content of this phase in sodium silicate-activated slag cements derived from slags with $13.2 \geq \text{mass\% MgO}$ (Bernal et al., 2014b; Le Saoût et al., 2011) (Figure 3B), except for the SEM-EDS datum at $\sim 7.8 \text{ mass\% MgO}$ (Ben Haha et al., 2012) and the ^{29}Si MAS NMR datum at 1.2 mass\% MgO (Al/Si ≈ 0.2) (Bernal et al., 2014b). This discrepancy can be partly attributed to the incomplete description of solid phases in the thermodynamic database, which would be particularly relevant for the datum at 1.2 mass\% MgO , as gismondine and/or N-A-S(-H) gel (which is thought to be a poorly-ordered zeolite-type phase (Provis et al., 2005)) were identified as reaction products in the cement studied by Bernal et al. (2014b). Simulations of NS-AS cements show that Ca-heulandite and natrolite are predicted for slags with $\leq 41 \text{ mass\% CaO}$ (Figure 4), in good agreement with this analysis and the identification of zeolites in these materials (Bernal et al., 2011; Bernal et al., 2014b). The bulk CaO concentration is therefore a key parameter controlling the formation of zeolite-type phases in AAS-based cements. However, it is important to note that Ca-rich zeolites such as gismondine, which are expected to have relatively high stability in AAS-based cements, are not described in the thermodynamic database used here because reliable thermodynamic data for these phases are not always available (Wolery et al., 2007).

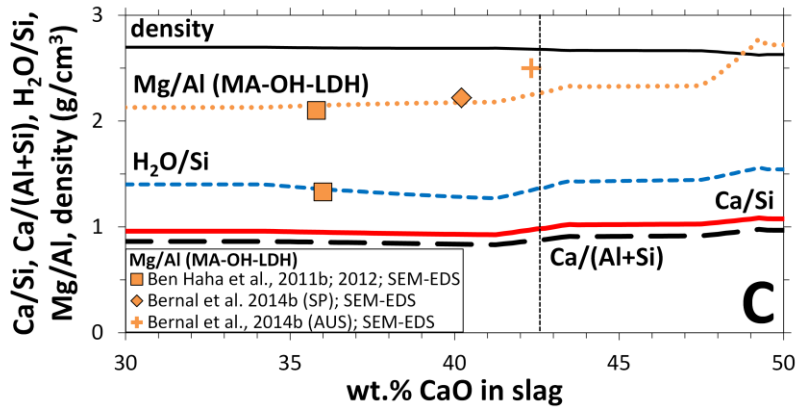
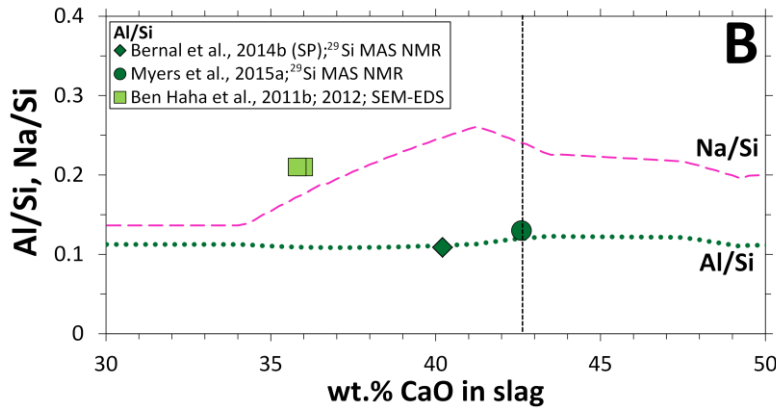
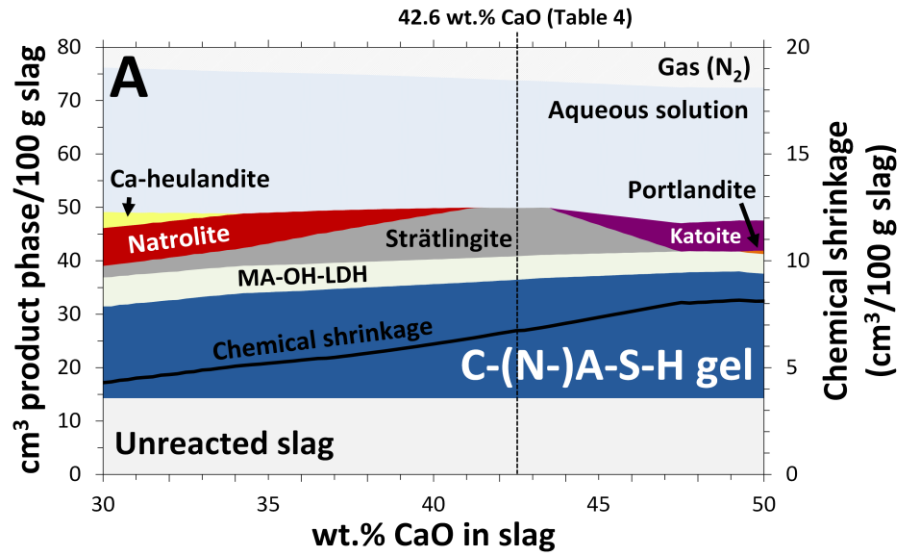


Figure 4. Simulated A) solid phase assemblages, B) Al/Si ratios in C-(N-)A-S-H gel, and C) Mg/Al ratios in MA-OH-LDH in NS-AS cements with bulk slag chemical compositions rescaled from Table 4 except for the Ca content, which is varied here (traces). Changes in B) Na/Si, C) H₂O/Si, Ca/Si and Ca/(Al+Si) ratios in C-(N-)A-S-H gel, and C) C-(N-)A-S-H gel density (g/cm³) are shown for visual reference. The symbols in B) and C) represent experimentally measured data for sodium silicate-activated slag cements derived from slag precursors with similar Al₂O₃ and MgO content (12 < mass% Al₂O₃ < 14.1, 5.2 < mass% MgO < 7.7) to the slag represented by Table 4. The difference in intrinsic porosity within the full range of modelled CaO compositions is 3%.

It is also notable that the total binder (solid + aqueous phase) volume changes markedly as a function of the CaO content in the slag, which suggests that the bulk CaO concentration is also a key parameter influencing the chemical shrinkage properties of these materials; a difference of 3.8 cm³/100 g slag (Δ chemical shrinkage = 47%) is identified over the range $30 \leq \text{CaO} \leq 49$ mass%, with more chemical shrinkage predicted at higher slag CaO content (Figure 4A). Therefore, it is expected that chemical shrinkage in NS-AS cements can be reduced through the use of raw materials with lower CaO content. Simulated Mg/Al ratios of the MA-OH-LDH phase and Al/Si ratios of C-(N-)A-S-H gel are in close agreement with the experimental data, with the exception of the SEM-EDS data at a slag CaO content of ~36 mass% which likely contains some intermixed low-Mg high-Al phases (Taylor et al., 2010).

The modelling results presented here provide a satisfactory account of the experimental data and so give confidence in using the CNASH_{ss} and MgAl-OH-LDH_{ss} thermodynamic models to describe NS-AS cements over the most common ranges of slag compositions and activator doses used in AAS cements ($7 \leq \text{mass\% Al}_2\text{O}_3 \leq 13.7$, Figure 2, $5.2 \leq \text{mass\% MgO} \leq 13.2$, Figure 3, and $35.8 \leq \text{mass\% CaO} \leq 42.3$, Figure 4). Within this range, the model predictions are within ~0.04 units in the Al/Si ratios of the C-(N-)A-S-H gel and ~0.3 units in the Mg/Al ratios of the MA-OH-LDH phase.

3.2 Simulated reaction of a Na₂SiO₃-activated slag cement

Additional thermodynamic modelling analysis of NS-AS cements was performed by varying the slag reaction extent from 0-100%, in the presence of Na₂SiO₃ (8 g Na₂SiO₃/100 g slag), while holding the slag chemical composition constant (Table 4).

The predicted solid phase assemblage consists of C-(N-)A-S-H gel as the dominant reaction product, and additionally MA-OH-LDH (Mg/Al \approx 2), strätlingite, Ca-heulandite, brucite, natrolite and katoite (Figure 5A). Zeolites are only predicted for slag reaction extents <40% (i.e. effectively at low bulk CaO concentrations, consistent with Figure 4), which is less than the experimentally-determined slag

reaction extent for AAS cement after 1 day of curing (Myers et al., 2015a), and is relatively consistent with the experimental observation of only minor amounts of these phases in AAS cements (Bernal et al., 2011; Bernal et al., 2014b).

The prediction of MA-OH-LDH and strätlingite is in relatively good agreement with experimentally-determined solid phase assemblages in NS-AS cements (Ben Haha et al., 2012; Brough and Atkinson, 2002; Burciaga-Díaz and Escalante-García, 2013; Myers et al., 2015a; Wang and Scrivener, 1995), where Mg-Al LDH phases are often identified and the formation of AFm-type phases are likely, although the calculations here do markedly over-predict the amount of strätlingite formed compared to the experimental observations. Approximately constant proportions of the main hydrate phases (strätlingite, MA-OH-LDH and C-(N-)A-S-H gel) are predicted relative to the total reaction product volume at slag reaction extents exceeding 40%. The influence of the additional Si supplied by the activator is diluted as more slag reacts, as the activator is assumed to be fully dissolved in the mix water prior to contact with the slag, and so contributes more significantly to the chemistry of the reaction products when the degree of reaction of the slag is low. This means that the slag chemical composition, rather than the activator, controls the stable product phase assemblage at higher extents of reaction.

The chemical shrinkage in this system is predicted to be 11 cm³/100 g slag at complete reaction of the slag (an overall volume reduction of 15%, Figure 5A), which matches the chemical shrinkage quantified experimentally by Thomas et al. (2012) for a sodium silicate-activated slag cement (12.2 ± 1.5 cm³/100 g slag) and is close to the values modelled by Chen and Brouwers (2007) (11.5-13.9 cm³/100 g slag) at 100% degree of reaction of the slag. Therefore, thermodynamic modelling predicts significantly larger chemical shrinkage in NS-AS cements than measured in hydrated PC (~6 cm³/100 g cement reacted (Jensen and Hansen, 2001; Tazawa et al., 1995)).

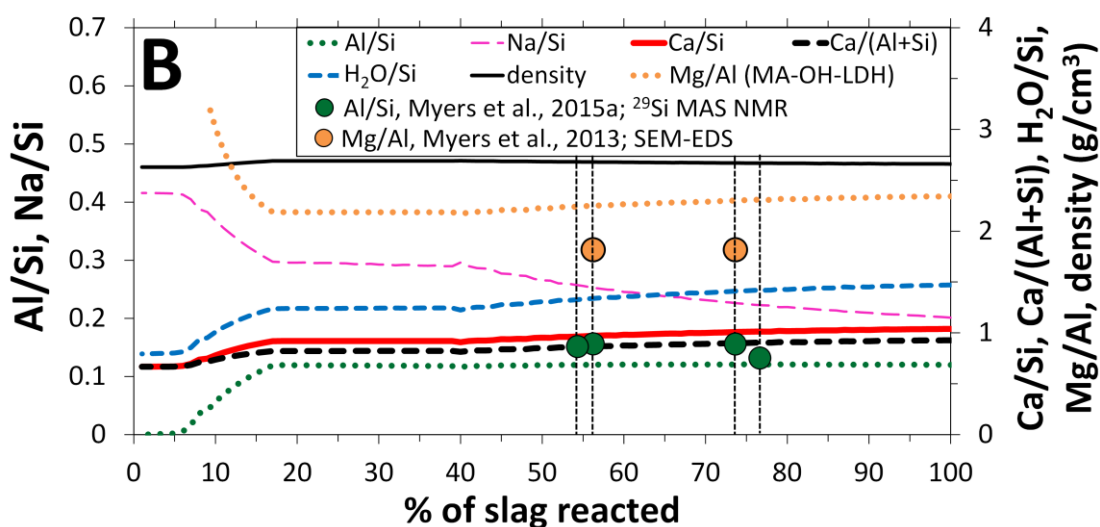
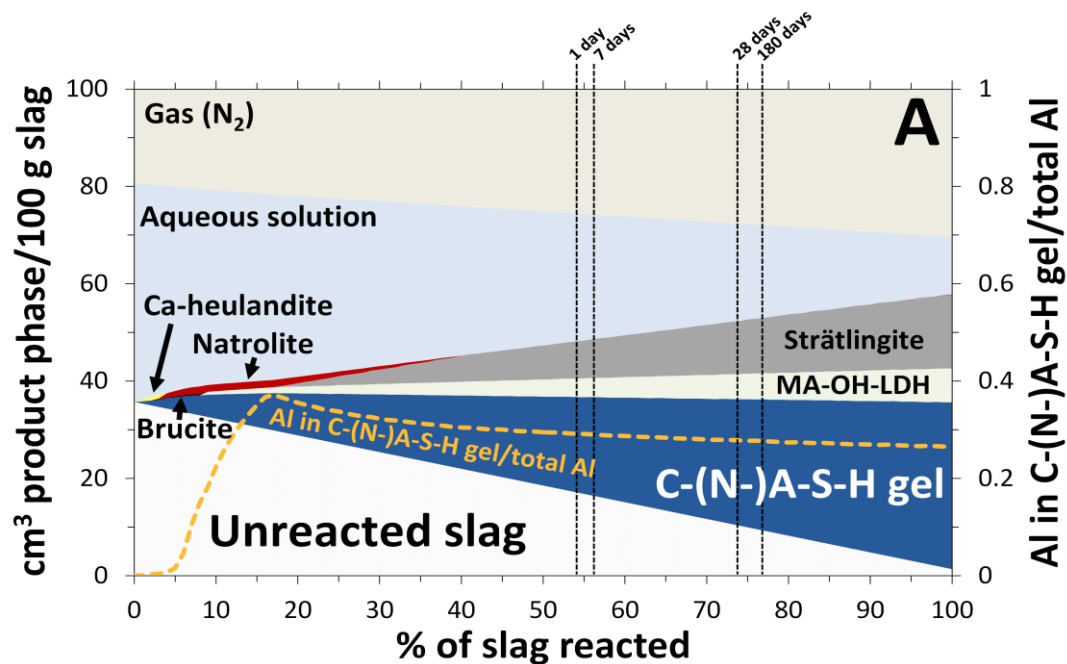


Figure 5. Simulated A) solid phase assemblages, and B) Al/Si ratios in C-(N-)A-S-H gel and Mg/Al ratios in MA-OH-LDH in an NS-AS cement using the slag chemical composition in Table 4. Changes in B) Na/Si, H₂O/Si, Ca/Si and Ca/(Al+Si) ratios in C-(N-)A-S-H gel, and B) C-(N-)A-S-H gel density (g/cm³) are shown for visual reference. The dashed vertical lines correspond to slag reaction extents determined experimentally at each time of curing (Myers et al., 2015a).

The increased Ca content and decreased Na/Si ratio of the C-(N-)A-S-H gel at higher slag reaction extents (Figure 5B) are reflected in the reduced bulk Si and Na concentrations and the relative decrease in the fraction of Na-containing end-members simulated as the alkali activation reaction progresses (Figure 6). A ~50% reduction in the concentration of Na in the pore solution is predicted from 0 to 100% slag reaction extent, although a constant pH of ~14 is maintained and >10 times more Na is always predicted to be present in the aqueous phase relative to C-(N-)A-S-H gel. The simulated

amounts of H₂O and Ca in C-(N-)A-S-H gel are directly linked via the end-member chemical compositions defined in the CNASH_{ss} thermodynamic model (Myers et al., 2014): the Ca-rich T2C* end-member (Ca/Si = 1.5) has a higher H₂O/Si ratio (= 2.5) compared to the Al and Na-containing end-members (H₂O/Si < 2, Table 1), and relatively more of this end-member is simulated at higher bulk slag reaction extents (Figure 6B). The simulated trends in pore solution element concentrations at >40% slag reaction extent (Figure 6A) are within ± 1 order of magnitude to those reported for NS-AS cement cured for 1-180 days (Gruskovnjak et al., 2006). More solubility data for NS-AS cement are needed to further assess the simulated pore solution compositions.

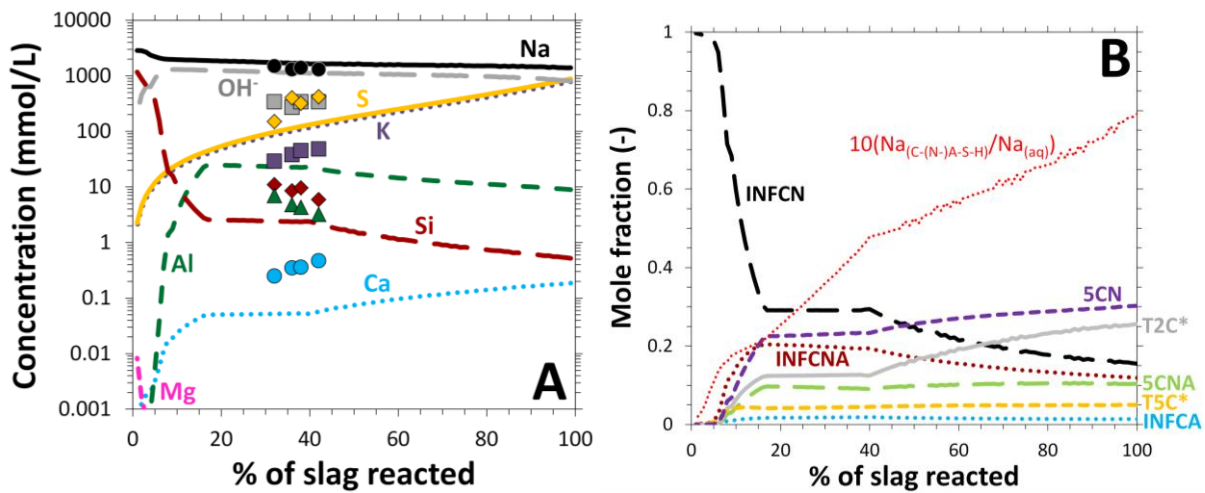


Figure 6. Simulated A) pore solution chemical compositions and B) end-member mole fractions and ratio of Na in C-(N-)A-S-H gel relative to Na in the aqueous phase (aq) for the NS-AS cement described by Figure 5. The mole fraction of the TobH* end-member is close to 0 over the full range of simulated slag reaction extents (not shown in B)). The symbols in A) represent sodium silicate-activated slag pore solution data reported by Gruskovnjak et al. (2006).

The simulated fraction of Al in MA-OH-LDH relative to the total amount of Al in the reaction products ($\text{Al}_{\text{MgAl LDH}}/\text{Al}_{\text{products}}$) is ~ 0.22 , which is consistent with deconvolution analysis of ²⁷Al MAS NMR spectra for the analogous experimental NS-AS cement between 1-180 days of curing ($\text{Al}_{\text{MgAl LDH}}/\text{Al}_{\text{products}} = 0.18\text{-}0.26$) (Myers et al., 2015a), but the predicted Mg/Al ratios are greater than those measured by SEM-EDS analysis for this material (Figure 5B). This result provides further support for explaining Mg/Al ratios < 2 in terms of intimately intermixed low-Mg high-Al phases with Mg-Al LDH phases, e.g. TAH or N-A-S(-H) gel, because the low Mg/Al ratio of this solid solution phase is 2

(Richardson, 2013). However, the simulations predict that the fraction of Al in C-(N-)A-S-H gel (Al_{CNASH}) relative to the total amount of Al in the reaction products ($Al_{CNASH}/Al_{products}$) is ~ 0.28 for slag reaction extents $>50\%$ (Figure 5A), which is much less than the relative amount of four-coordinated Al ($Al[4]$) assigned to the reaction products ($Al[4]/Al_{products}$) in ^{27}Al MAS NMR spectral deconvolution analysis of this NS-AS cement ($Al[4]/Al_{products} = 0.60-0.75$) (Myers et al., 2015a). These ratios, $Al_{CNASH}/Al_{products}$ and $Al[4]/Al_{products}$, would be comparable if C-(N-)A-S-H gel were the only major $Al[4]$ -bearing solid phase present in AAS cements (i.e. $Al_{CNASH}/Al[4] \approx 1$), but that is not the case here. Recent solubility results for C-(N-)A-S-H gel (Myers et al., 2015b) do not support any further increase in the stability of the Al-containing end-members in the CNASH_{ss} thermodynamic model, meaning that this discrepancy in the distribution of $Al[4]$ is probably due to other factors. These factors may include incomplete description of other $Al[4]$ -containing phases in the thermodynamic database used here, or that the discrepancy is founded in the experimental ^{29}Si and ^{27}Al MAS NMR analysis. Both options are now discussed.

The amount of strätlingite predicted by the thermodynamic modelling (Figures 2-5) was likely overestimated because this phase is not clearly distinguished in X-ray diffractograms of sodium silicate-activated slag cements cured for up to 3 years (Ben Haha et al., 2012; Burciaga-Díaz and Escalante-García, 2013; Wang and Scrivener, 1995), or in NS-AS/4 mass% PC blends cured for 3 years (Bernal et al., 2012). The solubility product used to describe this phase (Table 1) has an estimated uncertainty interval of ± 1 log unit derived directly from the scatter in the available solubility data for this phase (see Matschei et al. (2007) and references therein), and so an error in this value is unlikely to contribute significantly to the over-prediction of this phase. Therefore, it is likely that additional solid phase(s) are missing from the thermodynamic database used here (Table 1), which would be predicted to form in preference to strätlingite if they were present in the simulation. These may be zeolites such as gismondine and thomsonite (Bernal et al., 2011; Bernal et al., 2014b), or poorly ordered Q^4 -type N-A-S(-H) ('geopolymer') gels (Myers et al., 2013), each of which will accommodate Al in tetrahedral form and could account for the difference between the high tetrahedral fraction determined experimentally, and the notably lower tetrahedral fraction predicted in the current

simulations. Thermodynamic data are available for a large number of zeolites (see the compilation by Arthur et al. (2011) for example), but the large variety of possible chemical compositions and the availability of only a few data for each zeolite framework type (often only one datum), mean that more thermochemical or solubility data are needed to better define these phases in thermodynamic databases.

The maximum possible amount of Al[4] attributable to zeolites or N-A-S(-H) gel is, however, limited by the intensity of the ^{27}Al MAS NMR spectra of this NS-AS cement (Myers et al., 2015a) at ~60 ppm (relative to $\text{Al}(\text{H}_2\text{O})_6^{3+}$), which is the typical observed chemical shift at which Al[4] resonates in these phases (Davidovits, 1991; Duxson et al., 2007; Fyfe et al., 1982). Consequently, it is unlikely that zeolites and N-A-S(-H) gel can account for the large discrepancy between the modelled amount of Al[4] in C-(N-)A-S-H gel ($\text{Al}_{\text{CNASH}}/\text{Al}_{\text{products}} \approx 0.28$, Figure 5A) and the experimentally observed amount of Al[4] assigned to reaction products ($\text{Al}[4]/\text{Al}_{\text{products}} = 0.60\text{-}0.75$ (Myers et al., 2015a)). Further explanation for this discrepancy can be found in the assumption of congruent slag dissolution applied in the analysis of ^{29}Si and ^{27}Al MAS NMR spectra used as experimental data here (Bernal et al., 2014b; Myers et al., 2015a), which may not be fully attained in slag-based cements, and could significantly alter the deconvolution analysis presented due to the different lineshapes of partially reacted and unreacted slag (Dyson et al., 2007). Development of this understanding will be essential to further enhance the accuracy of the characterisation and simulation of the complex phase assemblages which are formed in AAS-based cements.

3.3 Simulated reaction of a Na_2CO_3 -activated slag cement

The reaction of a N $\bar{\text{C}}$ -AS cement is simulated via the same procedure used in the simulation of NS-AS cement discussed in section 3.2, except for the change in activator. The simulated solid phase assemblage contains C-(N-)A-S-H gel as the primary reaction product (Figure 7A). The additional products are $\text{C}_4\text{A}\bar{\text{C}}\text{H}_{11}$, MA-OH-LDH, calcite and natrolite. The prediction of calcite is consistent with the observation of CaCO_3 polymorphs in N $\bar{\text{C}}$ -AS cements cured for 20 months (Sakulich et al., 2010)

and 180 days (Bernal et al., 2015). Simulation of natrolite and Ca-heulandite is also in good agreement with the identification of heulandite and zeolite-A in N_C-AS cement (Bernal et al., 2015). The modelling results presented here and in section 3.3 are consistent with the identification of more prominent peaks for zeolites in X-ray diffraction patterns for N_C-activated (Bernal et al., 2015), compared to NS-activated, slag cements (Bernal et al., 2014b). C₄A₃H₁₁ has been identified in X-ray diffractograms of N_C-AS pastes cured for 1 day and for 540 days (Shi et al., 2006), although this phase is not always observable (Bernal et al., 2015; Sakulich et al., 2010) due to its tendency to be present as intermixed (Richardson et al., 1994) and/or poorly crystalline structures (Wang and Scrivener, 1995). The simulated chemical shrinkage extents for N_C-AS (Figure 7) and NS-AS cements (Figure 5) at 100% slag reaction extent are comparable, at 11 cm³/100 g slag.

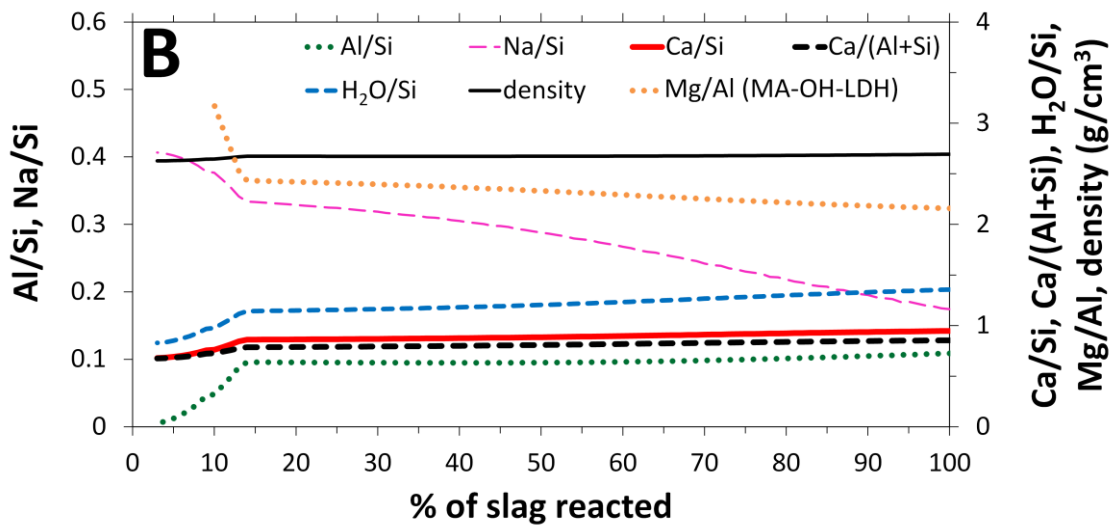
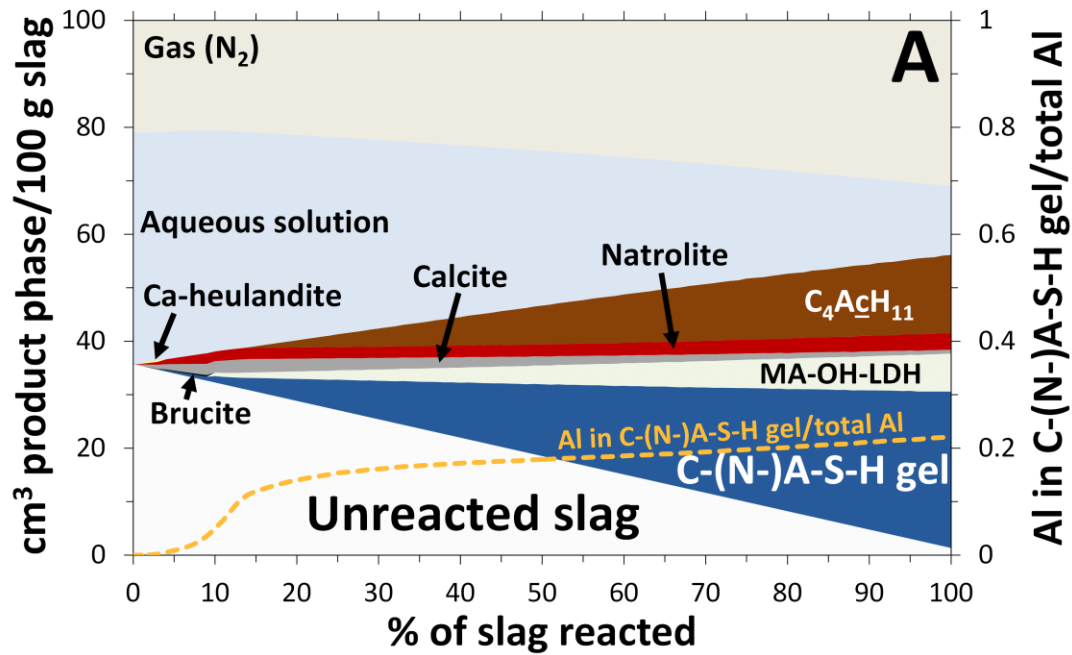


Figure 7. Simulated A) solid phase assemblages and B) C-(N-)A-S-H gel chemical compositions and densities (g/cm^3), and Mg/Al ratios in MA-OH-LDH in an N_c-AS cement using the slag chemical composition in Table 4.

Mg-Al LDH phases are experimentally observed in N_c-AS cements after 180 days (Bernal et al., 2015) and 55 days (Sakulich et al., 2009) of curing, in good agreement with the predicted phase assemblage (Figure 7A). Here, MA- \bar{c} -LDH is not predicted despite the high availability of CO₂, demonstrating the very high stability of MA-OH-LDH under the pH \geq 13 conditions in a hardened N_c-AS cement. Further clarification of this result is needed because recent ²⁷Al MAS NMR results for superficially carbonated NS-AS cements (Myers et al., 2015a), and carbonation depth analysis of

these materials after exposure to air for 16 months (Bernal et al., 2014b) can be interpreted in support of the formation of Mg-Al LDH phases intercalated with CO_3^{2-} . Detailed assessment of solubility and thermochemical data for Mg-Al LDH phases intercalated with OH^- and CO_3^{2-} (Bennett et al., 1992; Gao and Li, 2012; Johnson and Glasser, 2003; Morimoto et al., 2012; Rozov et al., 2011) indicates that the solubility product used to describe the $\text{Mg/Al} = 2$ MA-OH-LDH end-member of the MA-OH-LDH_{ss} thermodynamic model here may be in error by as much as several log units (Figure 1) and demonstrates the need for further studies of the thermodynamic properties of Mg-Al LDH phases.

Gaylussite has been observed in N_c-AS cement at early age (Bernal et al., 2015) but is not present in the solid phase assemblage simulated here (Figure 7); this phase is slightly undersaturated at low slag reaction extents at ~25°C (Bury and Redd, 1933; Königsberger et al., 1999). This difference indicates that kinetic factors enable the formation of gaylussite in N_c-AS cement cured at room temperature, and this is consistent with its observed consumption as the reaction proceeds (Bernal et al., 2015).

3.4 Phase diagrams for alkali-activated slag-based cements

The prediction of several reaction products in the simulated AAS cements is consistent with the bulk chemical composition of the mixes, which generally lie outside the composition envelope of phase-pure C-(N-)A-S-H gel (Figure 8).

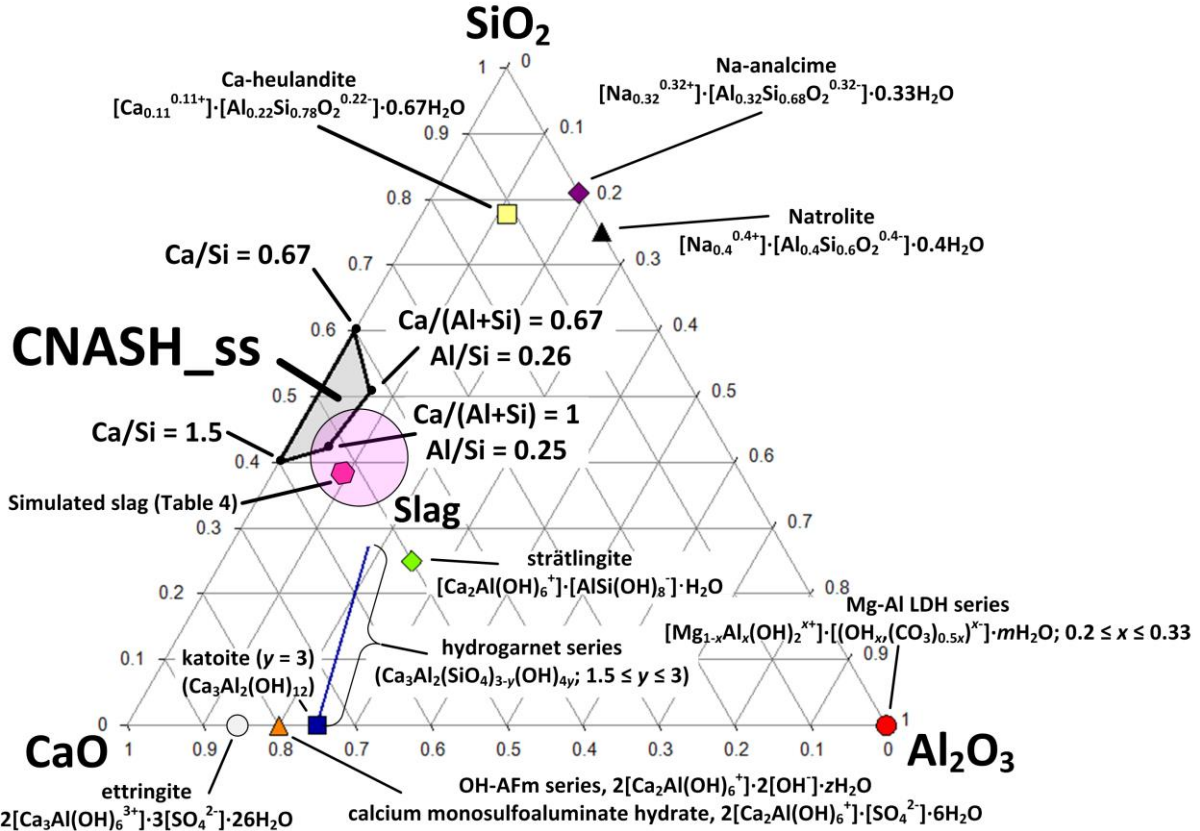


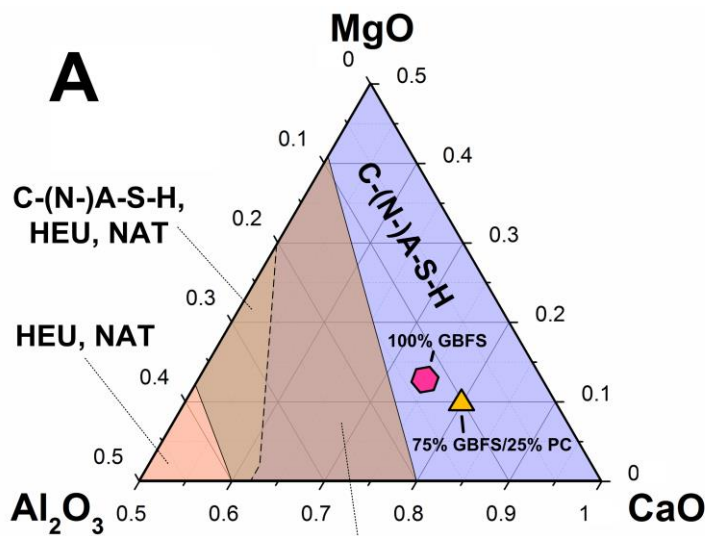
Figure 8. Projection of the chemical composition of some reaction products in AAS-based cements onto the CaO-SiO₂-Al₂O₃ ternary system. The grey and pink shaded regions are the composition range described by the CNASH_{ss} thermodynamic model for C-(N-)A-S-H gel (Myers et al., 2014), and the typical bulk chemical composition range of slag, respectively. The simulated slag described in Table 4 is represented by the pink hexagon.

Further analysis of AAS cement chemistry is performed by simulating phase diagrams at a fixed slag reaction extent of 60%, a constant amount of H₂S (equivalent in S content to a slag composition of 2 mass% SO₃, which is taken as a representative value of S content in slags studied in the literature (Ben Haha et al., 2011a; Bernal et al., 2014b; Gruskovnjak et al., 2006; Puertas et al., 2011; Richardson et al., 1994; Shi et al., 2006)) and slag compositions of either 30 or 40 mass% SiO₂, with the remaining chemical composition specified in terms of CaO, Al₂O₃ and MgO only. The CaO-Al₂O₃-MgO composition range selected here was chosen to represent the bulk chemical composition range relevant to AAS-based cements.

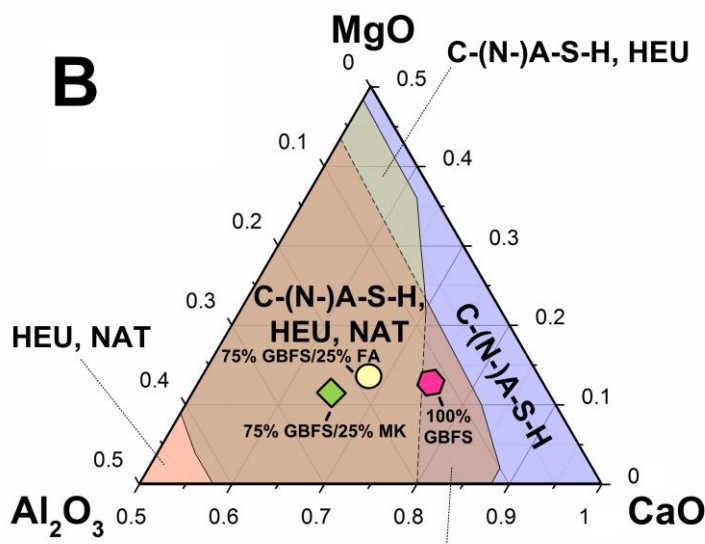
Zeolites are predicted in every phase diagram for the AAS cements simulated (shown for NS-AS cements only in Figure 9), and are more prominent at higher Si (i.e. lower Ca) and Al concentrations, but only Ca-heulandite and natrolite are predicted among the zeolites included in the thermodynamic

database (Table 1). The CaO-Al₂O₃-MgO composition region where C-(N-)A-S-H gel and zeolites are both simulated indicates where C-(N-)A-S-H and N-A-S(-H) gels are likely to coexist in AAS cements, due to the fundamental similarities of zeolites and N-A-S(-H) ('geopolymer') gels (Provis et al., 2005). Inclusion of reliable thermodynamic data for N-A-S(-H) gel and zeolites will be necessary to clarify the chemical compositional envelope in which these gels can coexist. The prediction of zeolites here, in both the higher pH ((NH)_{0.5}-AS) and lower pH systems (N_C-AS), Figures 7 and 9, indicates that increasing pH does not destabilise these phases and the corresponding N-A-S(-H) gel in favour of C-(N-)A-S-H gel in the pH and chemical composition range relevant to cements, as was proposed previously by García-Lodeiro et al. (2011). The increased stability of zeolites at lower CaO content (Figure 4), or alternatively higher Si and Al concentrations (Figure 9) – i.e. decreasing CaO/(Al₂O₃ + SiO₂) – demonstrates that control of Ca-Al-Si compositions is needed to form alkali-activated cements with mixed C-(N-)A-S-H and N-A-S(-H) gels (Ismail et al., 2014). Figure 9 shows that mixtures of C-(N-)A-S-H gel and zeolites are expected to be stable in Na₂SiO₃-activated 75 mass% GBFS/25 mass% fly ash (FA) (overall precursor SiO₂ content = 41 mass% based on the FA chemical composition from (Bernal et al., 2013)) or metakaolin (MK) cements (overall precursor SiO₂ content = 38 mass% based on the MK chemical composition from (Bernal et al., 2011)), but not in a hybrid system of Na₂SiO₃-activated 75 mass% GBFS/25 mass% PC (based on a PC chemical composition of 19.7 mass% SiO₂, 63.2 mass% CaO, 1.85 mass% MgO, 4.7 mass% Al₂O₃, 3.35 mass% SO₃ (Lothenbach and Winnefeld, 2006)). Figure 9 also shows that the stability of zeolites, and therefore of N-A-S(-H) gels, in NS-AS cement depends greatly on the slag SiO₂ content.

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Figure 9. Phase diagrams for NS-AS-based cement systems with overall precursor chemical compositions of 2 mass% SO_3 equivalent and A) 30 mass% SiO_2 and B) 40 mass% SiO_2 , with only the regions of stability for C-(N-)A-S-H gel and zeolites shown (Mg-containing phases are also typical reaction products: MA-OH-LDH at moderate and high Al_2O_3 content ($\text{Al}_2\text{O}_3/(\text{CaO}+\text{Al}_2\text{O}_3+\text{MgO}) > 0.1$); and brucite at moderate and low Al_2O_3 concentrations ($\text{Al}_2\text{O}_3/(\text{CaO}+\text{Al}_2\text{O}_3+\text{MgO}) < 0.25$)). See text for the GBFS, FA, MK and PC chemical compositions used. The w/b ratio is 0.4, the overall precursor reaction extent is 60% and the units are in mole fraction.

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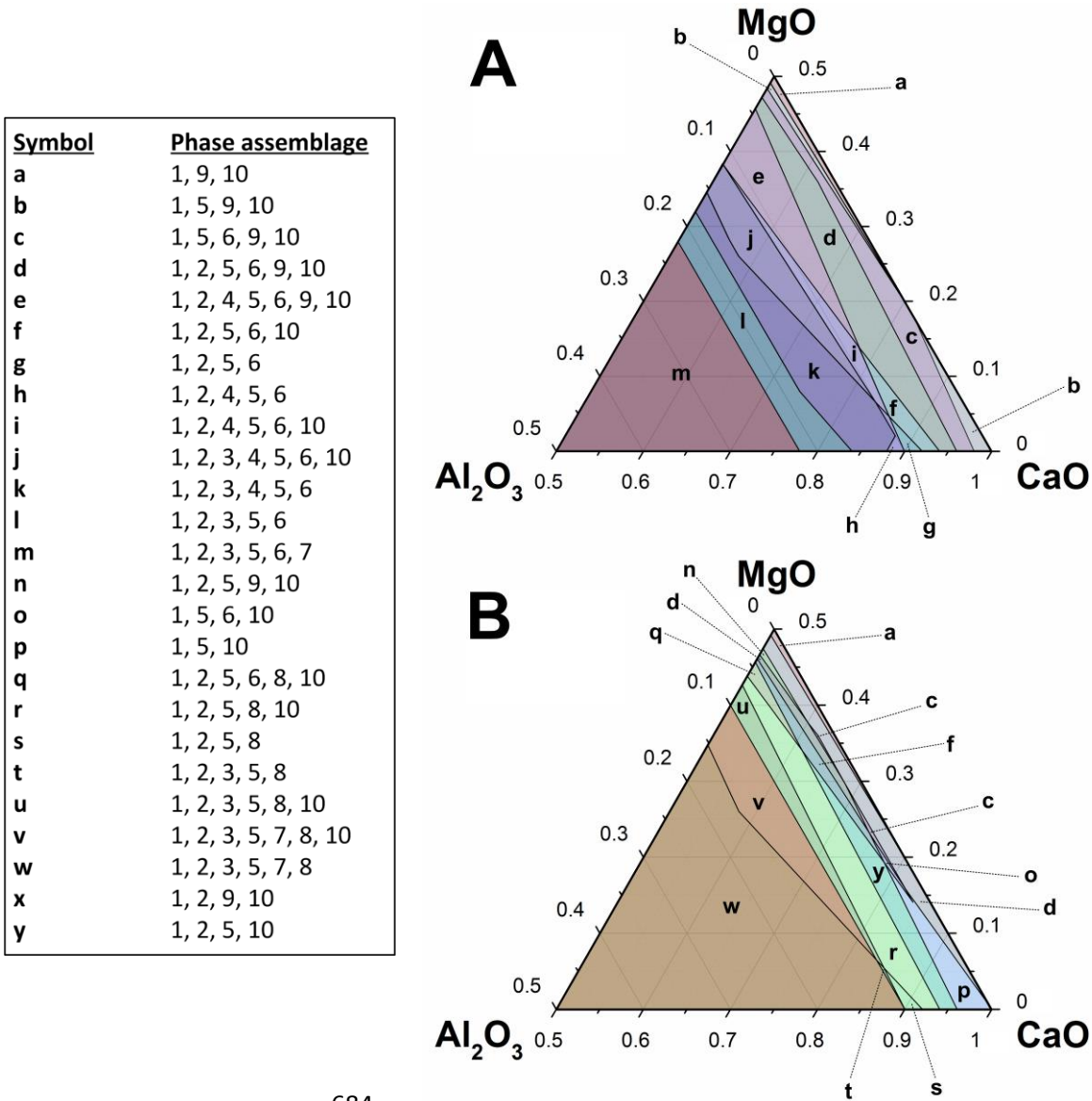
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Simulated phase diagrams for $(\text{NH})_{0.5}$ -AS-based cements are shown in Figure 10. The dominant solids in the simulated phase diagrams for $(\text{NH})_{0.5}$ -AS-based cements (Figure 10) are C-(N-)A-S-H gel and MA-OH-LDH. C-(N-)A-S-H gel is simulated over the full range of modelled $\text{CaO-Al}_2\text{O}_3\text{-MgO}$ compositions, and MA-OH-LDH is predicted everywhere in this composition range except at very low Al_2O_3 content ($\text{Al}_2\text{O}_3/(\text{CaO}+\text{Al}_2\text{O}_3+\text{MgO}) < 0.05$).

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685 Figure 10. Phase diagrams in the relevant bulk CaO-Al₂O₃-MgO composition range for (NH)_{0.5}-AS-
686 based cements with A) 30 and B) 40 mass% slag SiO₂ content, and 2 mass% SO₃ equivalent. The
687 phases are: 1, C-(N-)A-S-H gel; 2, MA-OH-LDH; 3, strätlingite; 4, katoite; 5, ettringite; 6, calcium
688 monosulfoaluminate hydrate; 7, natrolite; 8, Ca-heulandite; 9, portlandite; and 10, brucite. The w/b
689 ratio is 0.4, the slag reaction extent is 60% and the units are in mole fraction.
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691 Ettringite is predicted over a much larger range of CaO-Al₂O₃-MgO compositions than calcium
692 monosulfoaluminate hydrate. These phases are predicted to form here for slag with 2 mass% SO₃
693 equivalent but not for slag containing 0.8 mass% equivalent SO₃ (Table 4). Katoite is only present in
694 the phase diagrams for slags with 30 mass% SiO₂ in the (NH)_{0.5}-AS system. Portlandite is more
695 prominent in the 30 mass% SiO₂ (NH)_{0.5}-AS system (Figure 10A), but is only formed at relatively low

Al₂O₃ content ($\text{Al}_2\text{O}_3/(\text{CaO}+\text{Al}_2\text{O}_3+\text{MgO}) \leq 0.12$). Brucite is predicted in both phase diagrams, but not at high Al₂O₃ concentrations ($\text{Al}_2\text{O}_3/(\text{CaO}+\text{Al}_2\text{O}_3+\text{MgO}) > 0.2$). Natrolite and Ca-heulandite are the only zeolites simulated in the phase diagrams. Ca-heulandite has a larger stability region than natrolite in the 40 mass% SiO₂ system, but is not predicted at a SiO₂ content of 30 mass%, where only natrolite is simulated. However, the overall CaO-Al₂O₃-MgO composition region where zeolites are stable in (NH)_{0.5}-AS-based cements increases as a function of increasing slag SiO₂ content, which is consistent with the trends in zeolite stability described above for NS-AS-based cements (Figures 4 and 9). Similarly, the CaO-Al₂O₃-MgO composition range where strätlingite is stable is larger in the 40 mass% SiO₂ (NH)_{0.5}-AS cement system. These phases, strätlingite, natrolite and Ca-heulandite are only simulated for Al₂O₃/(CaO+Al₂O₃+MgO) ratios > 0.1, showing that intermediate to high Al concentrations are needed to stabilise these phases in (NH)_{0.5}-AS-based cements.

The phase diagrams presented here provide a framework for predicting solid phase assemblages in AAS cements, which can be improved with more relevant data, e.g. development of the thermodynamic database used (Tables 1-3). This work improves the way in which high-performance AAS-based cements can be designed, by linking the volumetric properties and solid phases formed in these cements to the raw materials used in their production. This framework also represents an important step towards predicting the durability of AAS-based cements, although further work is needed to link the key degradation mechanisms, e.g. carbonation, with the volumetric properties (Provis et al., 2012) and phase assemblages (Bernal et al., 2014b) in these cements.

4. Conclusions

This paper has presented a thermodynamic modelling analysis of AAS-based cements. The thermodynamic database used contains a CNASH_{ss} thermodynamic model for C-(N-)A-S-H gel, which explicitly describes Na and tetrahedral Al incorporated into this phase, a MA-OH-LDH_{ss}

ideal solid solution thermodynamic model for MA-OH-LDH, and thermodynamic data for some alkali carbonate and zeolite phases. The thermodynamic database presented here extends the utility of thermodynamic modelling in predicting the long-term chemistry of AAS-based cements, which is important for application of these materials, e.g. in the design of high performance cements for construction and in nuclear waste disposal applications, and further promotes the valorisation of metallurgical slags.

Thermodynamic modelling of NS-AS cements generally showed that the CNASH_{ss} thermodynamic model described the Al/Si ratios of the C-(N-)A-S-H gels formed in the most relevant composition range/alkali content for the majority of AAS cements. The Mg/Al ratios of the simulated MA-OH-LDH phase was generally in good agreement with experimental results for this phase in AAS cements, although additional thermodynamic data for MA-OH-LDH are needed to clarify the stability of this phase in carbonated and N_c -activated cement. Additional thermodynamic data for other reaction products such as TAH, zeolites and N-A-S(-H) gels are also needed for better consistency with the experimental Al/Si ratios in C-(N-)A-S-H gel and Mg/Al ratios in Mg-Al LDH. Simulated solid phase assemblages for NS-AS cements compared closely to the solid phases identified experimentally in these materials, and the simulations accurately predicted the experimentally measured chemical shrinkage in a NS-AS cement.

Phase diagrams for $(NH)_{0.5}$ -AS- and NS-AS-based cements were simulated, which showed that C-(N-)A-S-H gel and MA-OH-LDH are formed over the majority of chemical compositions relevant to these cements. Natrolite and Ca-heulandite featured more prominently in the phase diagrams at lower CaO concentration, and higher SiO_2 and Al_2O_3 content, indicating that the bulk $CaO/(SiO_2 + Al_2O_3)$ ratio plays a significant role in stabilising zeolites, and therefore N-A-S(-H) gels, in AAS-based cements. Zeolites were predicted to be stable in NS-activated 75 mass% GBFS/25 mass% FA and MK cements but not in hybrid NS-activated 75 mass% GBFS/25 mass% PC. Therefore, these phase diagrams can be used as a reference tool for the development of high-performance AAS-based

cements, by enabling solid phase assemblages for these cements to be predicted from the bulk compositions of the raw materials used.

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